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ONTARIO WATER

ANNUAL REPORT 1964

OWRC WATER POLLUTION CONTROL PLANTS

OPERATING SUMMARY

TD 367 .A56 097 1964 MOE

DIVISION OF PLANT OPERATIONS

Ontario Water Resources Commission

LABORATORY & RESTARCH FIBRERY MINISTRY OF THE ENVIRONMENT

TD 367 .A56 1964 operating summary : water pollution control plants.

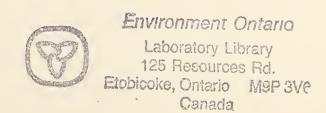
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097 1964

1964 OPERATING SUMMARY

Water Pollution Control Plants

ONTARIO WATER RESOURCES COMMISSION





PREFACE

The Division of Plant Operations has been operating water pollution control plants, since the Stratford plant (57-S-2) went into operation in June 1958.

Annual reports have been prepared by the Division at the end of each year on staffed projects which have been in operation for a full year. Standardization of the annual reports facilitates the comparison of operating data for the various projects operated by the Division.

The first summary report was prepared in 1963. It summarized and compared the operating data from 6 primary plants and 21 secondary plants including one total oxidation plant. During 1964, the number of plants increased and this report summarizes the operation of 9 primary plants and 29 secondary plants including 3 total oxidation plants. The diversity of treatment plants has permitted a comprehensive comparison of the various plants.



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2	Average Daily Flow		21	Operating Staff	63

PLANTS INCLUDED IN REPORT

PRIMARY

			Sludge Handling	Design Flow (MG)
1.	Belleville	61 -S- 84	Digestion	3.0
2.	Espanola	61-S-74	Digestion	0.665
3.	Fort Erie	59 - S-39	Digestion	1.8
4.	Fort William	61 - S-91	Digestion	6.0
5.	Owen Sound	60 - S-68	Digestion	3.0
6.	Point Edward	59-S-36	Digestion	0.57
7.	Port Arthur	58 -S-1 3	Digestion	4.0
8.	Sault Ste. Marie	59 - S-20	Vacuum Filtration	8.0
9.	Trenton	57 - S-4	Digestion	1, 0
	SECONDARY			
10.	Brampton	58-S-14	Digestion	2.0
11.	Brantford	58 -S- 11	Digestion, Vacuum Filtration	12.5
12.	Burlington D. L.	60-S-51	Digestion	2, 5
13.	Burlington E. G.	58 -S -28	Digestion	0.75
14.	Burlington Sky.	62-S-105	Total Oxidation	3, 125
15.	Comiston	57 -S- 8	Digestion	0.260
16.	Fergus	58 -S -23	Digestion	0.6
17.	Galt	61 - S-90	Digestion, Vacuum Filtration	5. 0
18.	Georgetown	58-S-17	Digestion	1.5
19.	Huntsville	58-S-15	Digestion	0.25
20.	Kingston Twp.	61-S-98	Digestion	0.83

21.	Kitchener	58-S-19	Digestion, Vacuum Filtration	13.5
22.	Lakeview	59-S-43	Digestion	5.0
23.	Markham Village	59-S-40	Digestion	0.334
24.	Moore Twp.	61-S-88	Total Oxidation	0.320
25.	Nepean Twp.	59 - S-35	Digestion	1.5
26.	North Bay	58-S-10	Digestion	4.0
27.	Orangeville	58-S-16	-	0.75
28.	Port Colborne E.S.		Digestion	0.85
29.	Port Colborne W.S.	59-S-47	Digestion	0.9
30.	Preston	59-S-46	Vacuum Filtration	1.8
31.	Richmond Hill	57-S-6	Digestion	1.6
32.	Simcoe	62-S-120	Digestion	1.40
33.	Sidney Twp.	62-S-121	Digestion	0.12
34.	Stratford	57 - S-2	Digestion	4.0
35.	Streetsville	57 - S-5	Digestion	0.8
36.	Tillsonburg	58-S-12	Digestion	0.67
37.	Waterloo	58-S-22	Vacuum Filtration	4.0
38.	Westminster	59 - S-33	Total Oxidation	0.25



GRIT REMOVAL

The average grit removal of 2.56 cubic feet per million gallons of sewage agreed with that experienced during 1963.

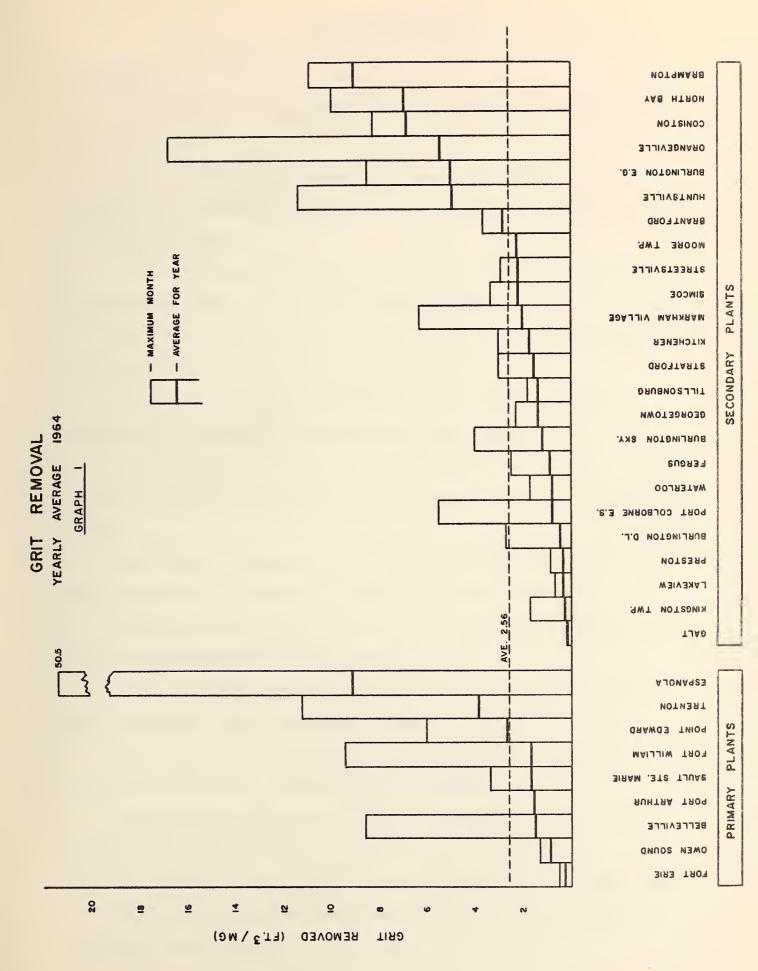
The amount of grit removed at 23 of the 33 plants was less than the average of 2.56 cubic feet per million gallons. Some of the plants such as Espanola received very large amounts of grit. Each plant has not been analysed to determine the reasons for large amounts of grit. In addition no analyses of the quality of the grit has been performed. In all cases the material settling in grit removal facilities has been considered to be grit.

The amounts reported herein, agree with those reported by others for typical treatment plants.

GRIT REMOVAL

(YEARLY AVERAGE) 1964

PRIMARY PLANTS	Cu. Ft./Mg. (FOR THE YEAR)	Cua FTa/Mga (FOR MAX. Mo.)
. Belleville	1.6	8.6
2. ESPANOLA *	9,1	50 . 5
3. FORT ERIE	0.2	0.4
	1 ₀ 8	
4. FORT WILLIAM **	0,9	9.4
5. OWEN SOUND		1.4
6. POINT EDWARD	2.7	6.0
7. PORT ARTHUR	1.7	2,5
8. SAULT STE, MARIE	1.8	3.4
9. TRENTON	3. 9	11.2
* Based on Estimated Flow ** Based on 6 months actual flow		
SECONDARY PLANTS		
10. BRAMPTON	9.0	10.8
II. BRANTFORD	2,8	3.7
12. BURLINGTON D.L. 60-S-51	0 . 5	2.7
13. BURLINGTON E.G. 58-S-28	5.0	8 . 5
14. BURLINGTON SKYWAY 62-S-105 *	1.2	4.0
15 CONTETON 58-S-8	6.8	8.2
15. CONISTON 58-S-8 16. FERBUS 58-S-23	0.9	2.5
17 GALT 61-S-00	0.1	0.1
17. GALT 61-S-90 18. GEORGETOWN 58-S-17	1.4	2.3
10 HINTONIES 58-5-15	4.9	11.3
19. HUNTSVILLE 58-S-15 20. KINGSTON TWP. 61-S-98	0,3	1.7
20 MENDS ON TWE 50-5-10	1.8	3.0
21. KITCHENER 58-S-19 22. LAKEVIEW 59-S-43	0.4	0.7
22 Markey Value 50 5 40		
23. MARICHAM VILLAGE 59-S-40	2,0	6 . 3
24, Moore Twr. 61-S-88 ** 25, Nepean Twp. 59-S-35	2.2	2,6
20. NEPEAN IWP. 09-3-30	UNAVAILABLE	UNAVAILABLE
26. North Bay 58-S-10 27. Grandeville 58-S-16	6.9	9.9
	5 . 4	16.8
28. PORT COLBORNE E.S. 29. PORT COLBORNE W.S. 59-S-47	0.8	5 _€ 6
30. PRESTON 59-S-46	(i.e.4.	0.0
31. RICHMOND HILL 57-5-5	UNAVAILABLE	UNAVAILABLE
* Based on 4 months actual flows ** Pro-rates on 9 months actual fl	Ows	
52. SIENEY TWF. 62-5-121	UNAVAILABLE	UNAVAILABLE
	2.1	3.4
33. SINCOS 62-S-120 34. STRATFORD 57-S-2	1.6	3,0
35. STREETSVILLE 57-S-5	2.1	2,9
35. STREETSVILLE 57-S-5 36. TILLSONBURG 58-S-12	1.4	801
37. WATTERLOO 58-S-22	0.8	1.7
37. WATERLOO 58-S-22 38. WESTMINISTER 59-S-33	UNAVAILABLE	UNAVAILABLE





PLANT LOADINGS

HYDRAULIC

The flow data for the primary plants is given in Table No. I and for secondary plants in Table No. II.

Table No. I shows that the Owen Sound, Belleville and Port Arthur plants had an average daily flow greater than design capacity. These three plants represent 38% of our primary plants.

The Owen Sound plant was overloaded 50 percent of the time, and had a maximum daily recorded flow 144 percent above design capacity.

The Belleville plant was overloaded 95 percent of the time and had a maximum daily recorded flow 171.1 percent above design capacity.

The Port Arthur plant was overloaded 67 percent of the time and had a maximum daily recorded flow 100 percent above design capacity.

Table No. Il shows that the Brampton-Chinguacousy, Galt, Lakeview, Nepean Township and Sidney Township plants had an average daily flow greater than design capacity.

The Brampton-Chinguacousy plant was overloaded 70 percent of the time and had a maximum daily recorded flow 80 percent above design capacity.

The Galt plant was overloaded 50 percent of the time and had a maximum daily recorded flow 58 percent above design capacity.

The Lakeview plant was overloaded 87 percent of the time and had a maximum daily recorded flow 70 percent above design capacity.

The Nepean Township plant was overloaded 80 percent of the time and had a maximum daily recorded flow 117 percent above design capacity.

The Sidney Township plant was overloaded 100 percent of the time and had a maximum daily recorded flow 230 percent above design capacity.

These 5 hydraulically overloaded plants represent 17% of our secondary plants.

Graph No. 1 indicates the average daily flow of each plant during 1964 as a percent of the design capacity.

TABLE I

O.W.R.C. WATER POLLUTION CONTROL PLANTS

PRIMARY PLANTS

HYDRAULIC, BOD AND SUSPENDED SOLIDS LOADINGS

1964

REMARKS								No Samples	
LOADING AS % OF DESIGN BOD S.S	47.2	24.4	54.0	37.5	91.9	247.3	91.9 101.3	1	59.8
LOAD % OF BOD	44.7	22.4	38.0	23.2	52.2	95.8	91.9	ı	30.2
AVG, DAILY FLOW FOR PEAK MTH MGD.	.194	ı	.930	1.420	4.200	5,830	6.300	4.100	10.100
MAX.DAILY FLOW RECORDED MGD.	.260	ı	1.380	4.120	7.320	8.600	7.980	8,530	19.630
% OF TIME FLOW GREATER THAN DESIGN	-0-	ı	O	17	50	95	67	2	23
AVG.DAILY FLOW AS % OF DESIGN	32	89	50	58	104	171	113	37	83
AVERAGE DAILY FLOW MGD.	.182	.450*	. 503	1.050	3.134	5.136	4.510	2.240	6.650
DESIGN FLOW MGD.	0.570	0.665	1.000	1.800	3.000	3.000	4.000	000.9	8.000
PROJECT	POINT EDWARD	ESPANOLA	TRENTON	FORT ERIE	OWEN SOUND	BELLEVILLE	PORT ARTHUR	FORT WILLIAM	SAULT STE. MARIE

* Estimated

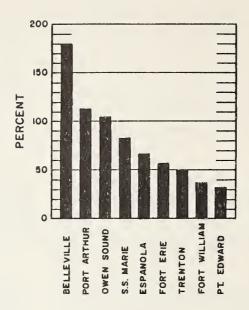
SECONDARY PLANTS

HYDRAULIC, BOD AND SUSPENDED SOLIDS LOADING

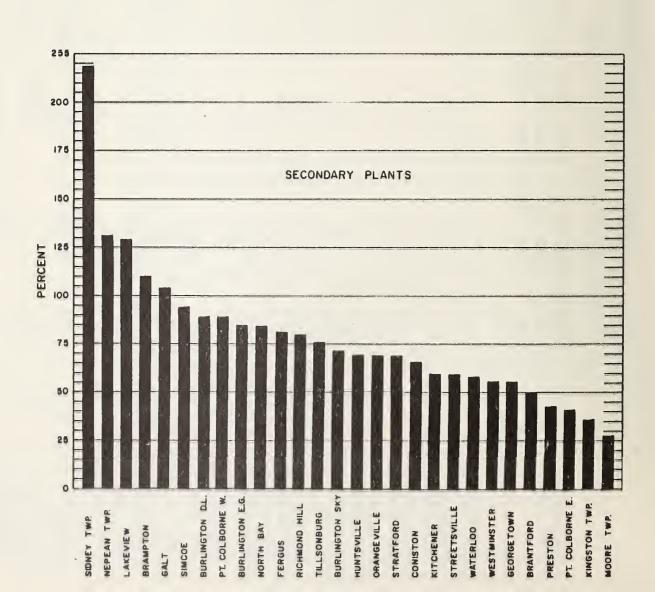
1964

			, *					
PROJECT DESIGN	NE	AC "	% OF TIME	MAX.DAILY	AVG, DAILY	LOADING	NG AS	REMARKS
FLOW M. G. J	DAILY FLOW	FLOW AS % OF DESIGN	THAN DESIGN	RECORDED	PEAK MTH	1	SS	
9				M, G, D,	M, G, D,			
Brampton 2.0		111	70	0	.45			
rantford 12.	9	49	-0-	. 78	.18	43.3	•	
urlington DL	2.26	06	45	•	3.020	φ.	2	
EG.	5 64	98	24	\sim	.21	2	2	
SKY 3		72	H	.16	. 28		7	
	6 .17	67	-1	0	19	٠ 0	3	
us.	0 .49	82	22	.31	57	ά	7	
alt 5.	5.178	104	50	. 89	2	7.	i.	
Georgetown 1.5	∞.	56	$2\frac{1}{2}$	7	.12	•	40.2	
wp.	3. 3	37	1,7,1	00.	9	ά	٠ 0	
	.1	69	25	.524	0	37.6	3	
13		61	-0-	-	20	ά		
5	6.4	129	87	2.42	.47	163.2	•	
Markham Village.3	34						No	accn
•	. 088	28	-0-	0	.095	9	8.3	flow data
n Twp. 1	1.98	132	80	3.252	.80	6		
Bay 4.	3,3	85	24	-	4	88.2	5	:
Orangeville .7	5 .51	69	7	,847	\vdash	9	49.4	
neE.	•	42	-0-	9	.549	*	» No	criteria
Port ColborneW . 9	80	68	35	. 75		œ œ	6 0 8 0	ON WW
Preston 1.8	.7	43	-0-	. 29	2		7	
Richmond Hill 1.6	.29	81	29	2.629	.61	7	4.0	
Simcoe 1.4	0 1.3	95		.92	1.610		7.7	New plant
Stratford 4.0	.72	89	22	. 50	4.060		2	7-110
Streetsville .8	00 .47	59	m	0		78.0	÷	
Sidney Twp.	.26	219	100	0	.280	0	2	
	. 65	77	7	. 693	, 566		8.99	alen del Theory
Waterloo 4.0	00 2.34	28	-0-	3,730	2,580	131.2	113.5	
Westminster .	250 .143	57	3	.276	.198	30.9	35.8	

AVERAGE DAILY FLOW AS PERCENT OF DESIGN FLOW GRAPH 2



PRIMARY PLANTS



BIOCHEMICAL OXYGEN DEMAND

Graph No. 3 indicates BOD loadings as a percent of design in descending order for both primary and secondary plants.

It can be seen that none of the primary plants is overloaded in BOD, but that seven or 25 percent of the secondary plants receive BOD loadings in excess of design.

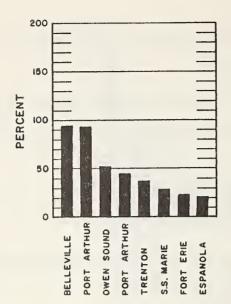
SUSPENDED SOLIDS

Graph No. 4 indicates SS loadings as a percent of design in descending order for both primary and secondary plants.

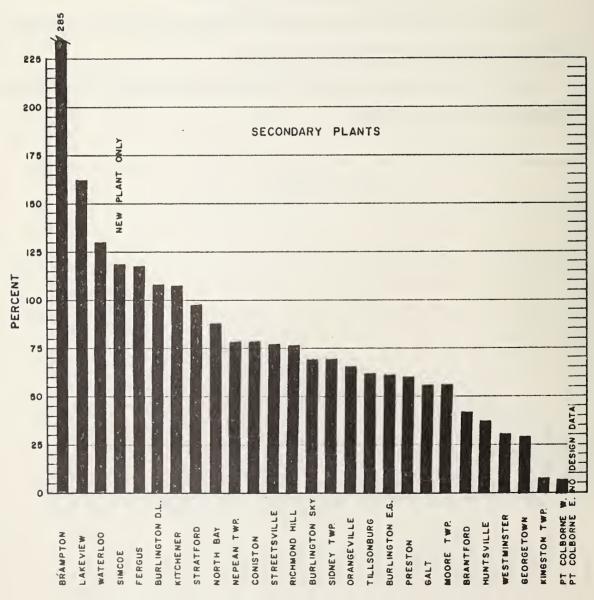
It can be seen that Belleville receives SS loads greatly in excess of design and that the Port Arthur SS loading is at design.

It can be seen that again seven or 25 percent of the secondary plants receive SS loadings in excess of design.

B.O.D. LOADINGS AS PERCENT OF DESIGN

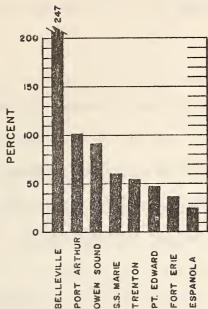


PRIMARY PLANTS

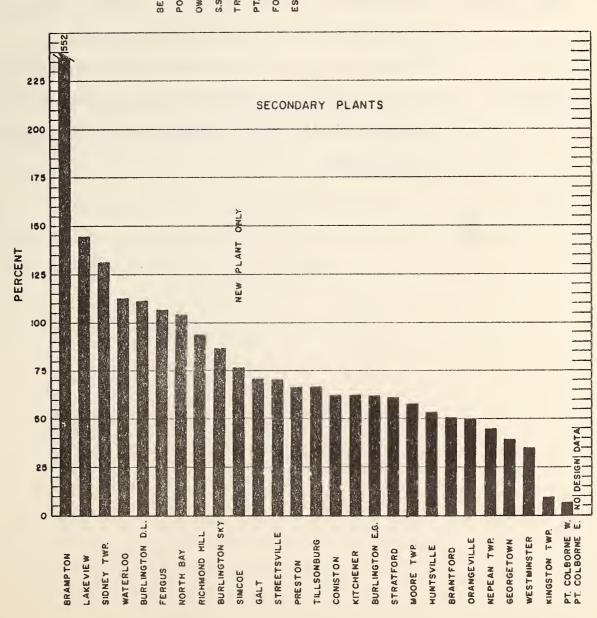


S.S. LOADINGS AS PERCENT OF DESIGN

GRAPH 4



PRIMARY PLANTS



OVERALL LOADINGS

A comparison of the graphs for flow, BOD and SS shows that the following plants are overloaded:

PRIMARY

Belleville - This plant has a very serious hydraulic overloading coupled with an extremely high SS load. The BOD loading is approaching design.

Port Arthur - This plant is at design capacity under all three criteria.

Owen Sound - The Owen Sound plant is at capacity from a hydraulic and SS aspect but its BOD load is only 50 percent of design.

SECONDARY

Sidney Township-This plant has a very serious hydraulic overloading coupled with a high SS loading. The BOD loading is relatively light.

Lakeview - This plant is very seriously overloaded under all three criteria.

Brampton - This plant is hydraulically overloaded and has excessive BOD and SS loadings. The BOD and SS loadings can best be described as fantastically high.

REMOVAL EFFICIENCY

Table No. III is a summary of the 1964 sampling results for all plants having an annual report.

PRIMARY PLANT REMOVALS

The concentrations of BOD and suspended solids of raw sewage and final effluent for all primary plants are shown on Table III and Graph 5. The average removal obtained was 47 percent for BOD and 62 percent for suspended solids compared to 45 and 64 percent for 1963. These efficiencies are above normally anticipated values of 25 to 35 percent for BOD and 50 to 60 percent for suspended solids.

The lowest efficiency of BOD removal was experienced at Point Edward (34%) and the highest at Belleville (62%). The lowest efficiency of suspended solids removal was noted at Fort Erie (39%) and the highest at Point Edward (78%).

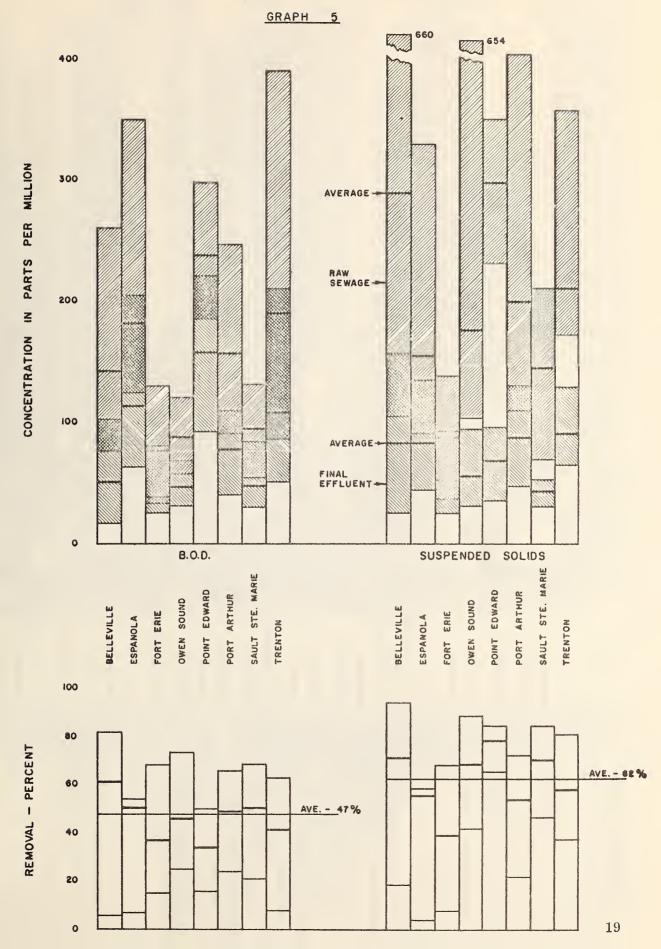
The average reduction of BOD and suspended solids at secondary plants was 92 and 90 percent respectively. This is consistent with results experienced by others and agrees with those noted for 1963.

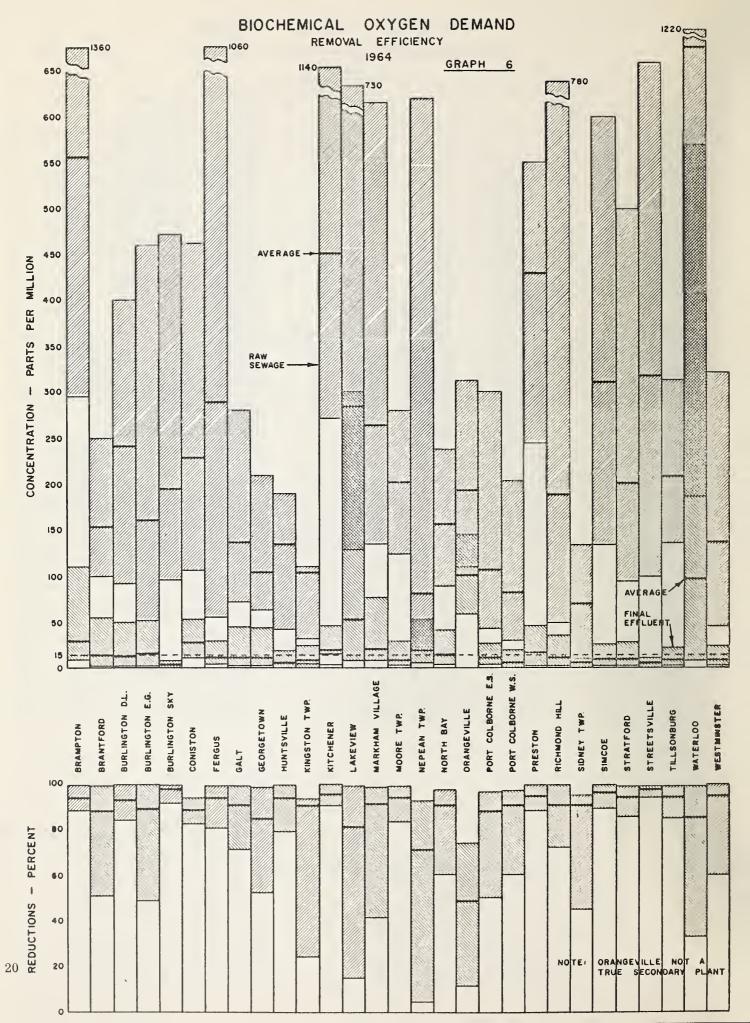
REMOVAL EFFICIENCY

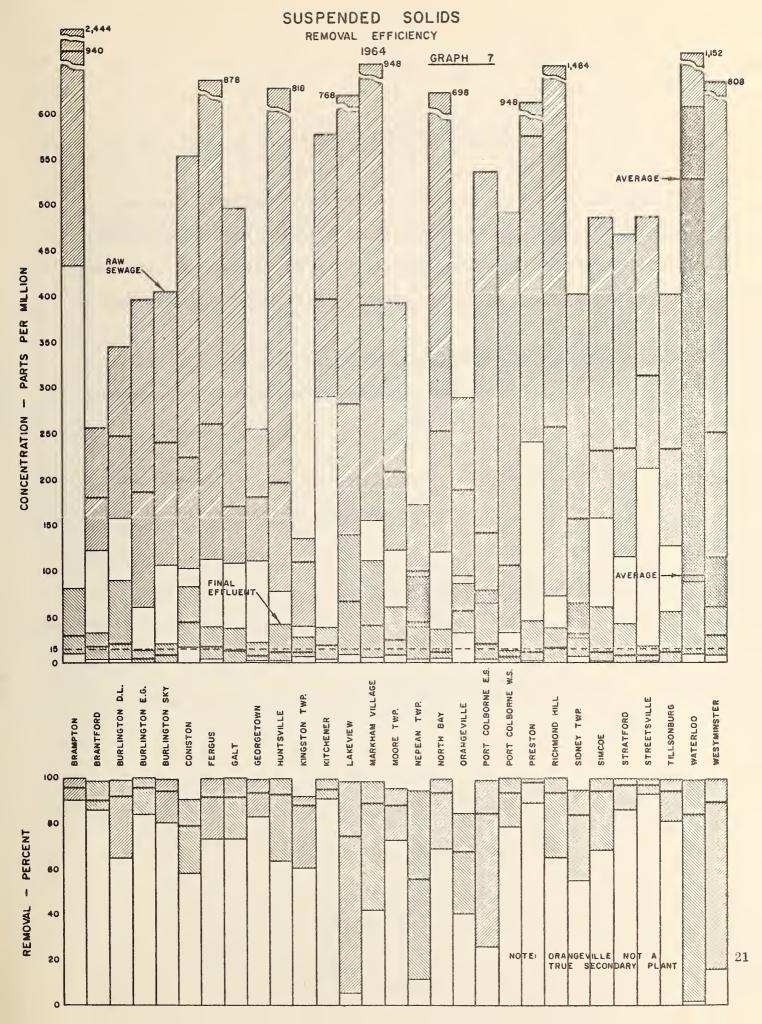
		В	TOCHEN	AICAL	0xyge	N DEM	AND					Sus	PENDEI	SOLI	DS	-		
PROJECT		RAW PF	М	FIN	AL PF	M	REMO	VAL %		R	AW PF	M	FIN	IAL PF	M	REMO	VAL %	
PRIMARY	MAX	MIN	AV.	MAX	MIN	Av.	MAX	MIN	AV.	MAX	MIN	Av.	MAX	MIN	AV.	MAX	MIN	Av.
1 . BELLEVILLE 2 . ESPANOLA 3 . FORT ERIE 4 . FORT WILLIAM 5 . OWEN SOUND 6 . POINT EDWARD 7 . PORT ARTHUR 8 . SAULT STE MARIE 9 . TRENTON	260 350 130 - 120 295 245 130 390	76 125 34 57 185 90 54 86	140 181 76 - 86 238 147 95 189	102 205 78 66 220 114 82 210	18 62 28 32 92 40 32 51	54 1 15 37 46 157 77 47 109	81 54 68 - 73 50 66 68 62	6, 7 15 26 16 24 20 8	62 54 37 46 34 48 50 42	660 329 138 - 654 352 404 210 358	104 90 24 - 102 232 112 68 172	289 155 84 - 176 296 198 144 212	158 134 88 - 96 95 128 53 127	24 42 38 30 36 44 36 64	82 83 51 57 66 87 43 91	93 59 68 - 88 84 72 84 80	18 4 7 42 66 21 47 37	72 59 39 68 78 56 70 57
AVERAGE	240	88	144	135	44	80	65	1 5	47	388	113	194	110	39	70	78	30	62
SECONDARY																		
10. BRAMPTON 11. BRANTFORD 12. BURLINGTON DL 13. BURLINGTON EG 14. BURLINGTON SKY 15. CONISTON 16. FERBUS 17. GALT 18. GEORGETOWN 19. HUNTSVILLE 20. KINGSTON TWP. 21. KITCHENER 22. LAKEVIEW 23. MARKHAM VILL. 24. MODRE TWP. 25. NEPEAN TWP. 26. NORTH BAY 27. ORANGEVILLE 28. PORT COLBORNES 29. PORT COLBORNES 30. PRESTON 31. RICHGOND HILL 32. SIDNEY TWP. 33. SINGOE 34. STRATFORD 36. STREETSVILLE 36. TILLGONSURG 37. WATERLOO 38. WESTMINISTER	205 550 780 136 600 500 660 315 1220 320	295 100 90 50 95 106 54 74 63 44 270 136 125 22 88 110 44 30 245 50 125 135 100 135 185 48	567 154 242 161 195 229 289 139 106 136 109 451 285 264 203 84 157 194 108 83 428 197 311 201 318 212 676 135	114 58 51 51 9 54 29 46 46 20 25 46 20 25 47 30 21 47 30 21 47 30 21 26 27 28 21 24 57 25 26 27 27 28 28 28 28 28 28 28 28 28 28 28 28 28	933320523-747845355534433322272	31 18 17 18 4 29 14 6 10 10 14 6 10 10 10 10 10 10 10 10 10 10 10 10 10	98 98 99 99 93 98 98 99 98 98 99 98 97 74 97 99 96 99 98 99 99 99 99 99 99 98 99 98 99 99	88 52 84 48 91 82 80 71 52 78 84 42 60 87 84 84 84 84 86 86 86 86 86 86 86	- 48 87 96 96 92 97 95 95 95 86 95	2444 256 346 396 404 552 878 494 254 813 7576 768 948 388 172 694 288 532 486 948 400 452 462 462 462 484 400 1152 808	432 124 156 60 106 108 116 76 42 288 140 152 124 38 120 94 60 32 232 71 252 112 210 126 60	940 182 249 182 246 226 262 172 180 194 114 282 208 100 250 181 142 103 549 256 229 230 311 231 526 250	80 36 88 15 21 84 43 40 22 42 30 40 22 42 350 114 66 60 47 41 66 60 416 60 60 614 60 60 614 60 60 60 60 60 60 60 60 60 60	9551-05122049882463-2-62-3225	30 18 20 7 12 47 19 15 12 14 20 7 14 25 43 14 57 21 6 3 16 8 13 16 8 18 29	99 97 98 99 99 99 99 97 98 99 97 98 96 94 98 84 98 84 99 99 99 99 99 99 99	90 86 65 84 80 57 73 72 83 63 60 90 5 42 72 12 68 40 26 78 54 65 84 93 80 80 80 81 81 81 81 81 81 81 81 81 81 81 81 81	97 99 96 95 97 98 97 98 97 98 97 98 97 98 97 98 97 98 97 98 98 97 98 98 98 98 98 98 98 98 98 98 98 98 98
AVERAGE	508	101	230	58	A,	17	98	66	92	644	123	269	74	Δ,	22	98	65	90°

LAREVIEW AND ORANGEVILLE HAVE BEEN OMITTED FROM AVERAGE. DURING 1364 THESE FLANTS ACT GIVING FULL SECONDARY TREATMENT.

BIOCHEMICAL OXYGEN DEMAND AND SUSPENDED SOLIDS REMOVALS



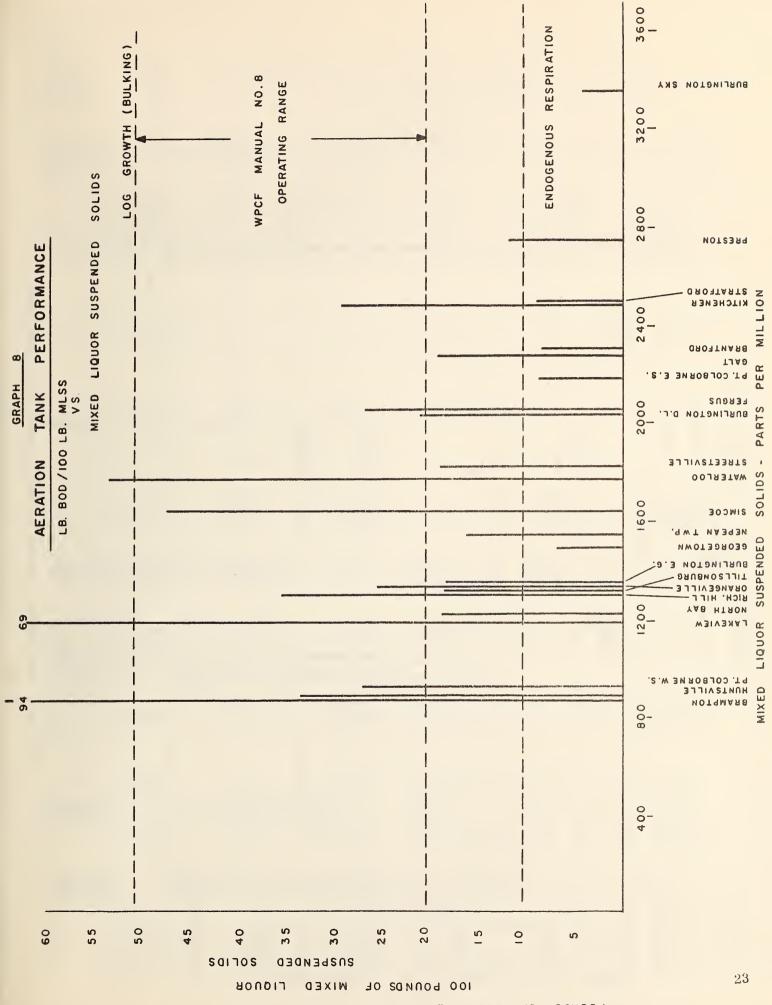


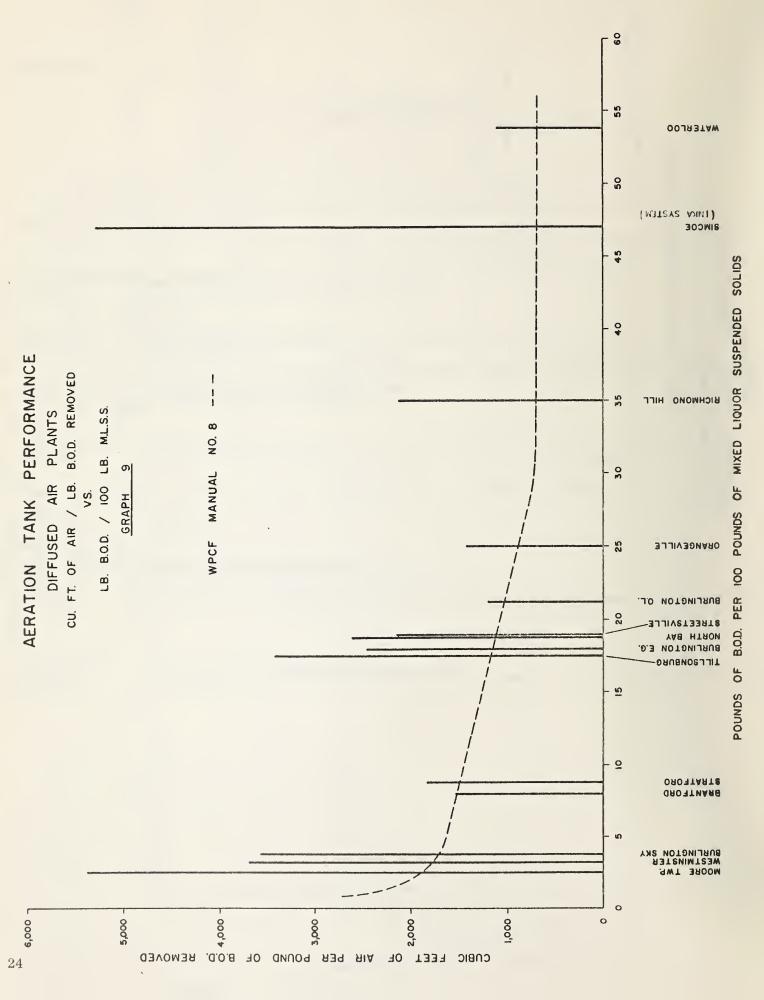


AERATION TANK PERFORMANCE

The loading applied to the aeration sections of the treatment plants is shown on Graph 8. The aeration sections of three plants (Brampton, Lakeview and Waterloo) were loaded beyond the 50 pounds of BOD, per 100 pounds of mixed liquor suspended solids figure. Expansion of all three of these plants is presently being planned or under construction.

Most of the plants experienced loadings on the aeration section below the ratio of 20 and as a result more air was used than is theoretically required for the amount of BOD reduced. This is shown on Graph 9.





	Mo.
	Detention Design At Max. Mo. Hrs. Flow 25% Return
	Design Hrs.
	Diffuser
	ft. ³ Air lbs. BOD Rem.
ORMANCE	lbs. BOD 100 lbs. MLSS
N TANK PERFORMANCE	Prim. Eff. lbs. BOD ft. Air D BOD 100 lbs. lbs. BOD ppm MLSS Rem.
ERATION	MLSS
Y	Actual Flow MGD
	Design Flow MGD
	Type
TABLE IV	Project

6.7	ì	5.0	4.3	0		5	5.8	0	6.12		ō		0	4.3	1	0		2.9	4.6	į	5		5.8		Q	5.7	9 6) 	ı	4.6		1	1	ı	1
10.2	9	0.9	9	31.7		4.4	7.0	8.0	6.75		. 7.5		b. &b	6.0	6.06	24.0		5.4	5.31		6.0		6.7		9. 7	5.9	9		7.68	5.7		6.1	10.1	7.2	24.2
Diffusers	Sparjers	Diffusers	Coliflex Diffusers	1500 -	Ceramic	A. C. 3	A. C. 20per	A. C. 8	Chicago	Pump 2	C. P. Disc-	ffusers	A, C, 56	Sparjers	Sparjers	C. P	Sparjers	A. C. 6	Diffusers	Diffusers	A. C. 4		A. C. 6		A. C. 6	Carbon-	Ceramic	Diffuser	1	Dome-	Diffuser	Diffuser	Sparjers	Sparjers	3
822	1524	1231	2487	3534		1	1	q	ı				ı	1209		5332		•	2598	1468	ī		!		ł	2143			5244	1894		2115	3458	1077	3700
94	00	21	18	4		26	19	_	33	1	Available		53	69	Available	2		16	19	25	œ		26		12	35	Available		7.2	6		19	18	54	က
203	110	150	114	195		178	108	89	143		Data. A		592	202	Data A	203		47	89	143	108		44		196	105	Data		195	88		215	136	592	135
865	2305	2020	1349	3344		2040	2369	1493	887		No		2497	1190	No	5517		1536	1223	1355	21.88		920		2743	1300	N	-	1631	2496		1858	1318	1780	4624
2, 214	6.070	2, 260	0.645	2.240		0.494	5, 192	0.840	0.173		0.310		8.260	6,445		0.088				0.514	0.359		0.804		0.780	1.290	0.980		1.326	2.720		0,470	0.512	2.340	0.143
2.000	12.500	2,500	0.750	3, 125		0.600	5.000	1.500	0.250		0.83		13.500	5.000	0.334	0.320		1.500	4.000	0,750	0.850		0.900		1.800	1.000	0 195		2.000	4.000		0.800	0.665	4,000	0.250
Single Pass	Triple Pass	Triple Pass	Single Pass	TO		Mech. aera.	Mech. aera.	Mech. aera.	Mech. aera.		Single Pass	,	Mech. aera.	Three Pass	Single Pass	TO		Mech. aera.	Single Pass	Single Pass	Mech. aera-	tion	Mech. aera-	tion	Mech. aera.	Single Pass	Sinolo Dass		Single Pass	Single Pass		Single Pass	Single Pass	Bisorbtion	ТО
Brampton	Brantford	Burlington DL	Burlington EG	Burlington SKY		Fergus	Galt	Georgetown	Huntsville		Kingston Twp.		Kitchener	Lakeview	Markham Vill.	Moore Twp.		Nepean Twp.	North Bay	Orangeville	Port Colborne -	ES	Port Colborne -	WS	Preston	Richmond Hill	Sidney Twn		Simcoe	Stratford		Streetsville	Tillsonburg	Waterloo	Westminister

Estimated

String and string and string and string string rate.

CHLORINATION

The chlorine dosages experienced at various plants are shown in Table $\,V\,$ and $\,$ Graph $\,10\,$.

In general the actual dosages agreed with those suggested in the WPCP Manual of Practise No. 8. However, very high dosages were experienced at Fort William, Point Edward and Trenton. The dosage at Point Edward was high as a result of low flows and the difficulty of maintaining a chlorine dosage matched to the low flow.

GRAPH

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SUMMARY	ı
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	COMMENTS			FLOW ESTIMATED													4 MONTHS! DATA								
	AV. CL. Dosage PPM		3,73			13.28	3,34	12,43	2,50	4.76	13,28		3,24	2,03	3,54	2.74	4,30		5,08	3.44	3,36			3,56	6.24
	MIN.CL. DOSAGE PPM		3,49	4	Z Z	88	2,39	10,65	1.97	2,92	6.14		1.85	0.64	2,86	1.74	3,63	4	2,40	2.82	2.42	4	∢	5,69	5. 12
4	MAX. CL Dosage PPM		4.04			15,49	3.94	13,48	2,93	5.80	17.44		4.34	2.40	4.56	4.54	4.98		8.14	3.80	4,49			69*7	7.32
9 6	TCTAL CHLORINE 185.		30114		8781	28045	20019	7647	22590	53824	10628		26223	17079	19162	6452	5952		9153	09159	10325			1076%	147 184
10 N DATA	TOTAL FLOW MG		1879,68		- 512,92	819.84	1147,207	929*99	1548,94	out-2432,62	184.23		810,463	- 2220,60	823.798	- 235,486	271,006		180, 124	1895, 161	307,116			3026,52	2358,770
CHLORINATION	Av. KETN. (FINS)		<u>∞</u>		23 + 0UT-	•	10.7	82	8	+ 8°-	74		4	10 + 0UT-	ר אנר -	- TOC + 21	י ארר		8	<u>e</u>	94			24	88
SUMMARY CHL	AV. DAILY FLOW NGD		5,30	0.45	1.05	2, 15	3, 15	0.18	4,40	6.50	0.50		2.2	6.07	2,26	0.64	2.24	C. 18	0.49	5.19	0.84	0.17		ස ්	4.0
SURA	MONTHS OF CHLORINE		ഹ	•	,ALL 6	ო	7	2	9	ALL 7	ω		21	LO LO	2	ALL 12	N	0	21	21	21	•	•	2	<u>2</u>
	DESIGN RETENTION (MINS)		8	•	13.4 + OUTFALL	å	5.	27	8	1.5 + OUTFALL	37		N	5+ OUTFALL	1	10 + OUTFALL	•	2	m	13.2	%	8	<u> </u>	<u>ഹ</u>	20
	DESIGN FLOW NGD		3.000	0,665	I.800	000°9	3,000	0.570	4.000	8.000	000*1		2.000	12,500	2,500	0.750	<u>8</u>	0.260	009°0	5,000	1.500	0,250	0.830	13,500	5,000
TABLE V	PROJECT	PRIMARY	belleville	ESPANOLA	FORT ERIE	FORT MILLIAM	OWEN SOUND	POINT EDWARD	PORT ARTHUR	SAULT STE, MARIE	TRENTON	SECONDARY	BRAMPTON	BRADFORD	BURLINGTON D.L.	BURLINGTON E.S.	BURLINGTON SKY.	Coviston	FERGUS	GALT	SEOPSETOWN.	HULTSVILLE	Kinsston Twe.	A 140 and 18 miles	LAKEN-EM

L. CONMENTS E	FLOW ESTIMATED													
AV. CL. DOSAGE PPM	4.49	7.40	2,69		6,67	3,08	5.62	7.21			3,50	5.00	9.27	5.26
MIN.CL. DOSAGE PPM	2.17	6.80	2.2		4.68	1.87	3,50	5,61			2.18	4,34	5.94	4.76
MAX.CL. DOSAGE PPM	5.41	8.90	3,50		8.51	6.37	9,43	8°6			5.1	5,68	₽.	60°9
TOTAL CHLORINE LBS.	2457	978	7385		12505	9064	15965	34026	۷ Z	∢ ×	3210	3738	79064	1330
TOTAL FLOW MG	84. 180	32,020	726.411	1234,328	187,373	294,212	284,326	472,211			172,302	187,461	852,937	52,469
AV. RETN.	75		<u>8</u>	ଷ	43.5	<u>®</u>	R	14			34	39.4	4	40.5
Av. DAILY FLOW MGD	0.23	60°0	8.	3,39	0.51	0.80	0.78	ଅ	0.28	F.33	0.47	0.51	2,34	0.14
MONTHS OF CHLORINE	ω	9	9	6 (APP)	12	21	21	12	4		თ	9	12	ſ
DESIGN RETENTION (MINS)	25	8	11	Ю	9°82	91	15	11,3	8	16.4	8	30.2	6	22.7
DESIGN FLOW MGD	0.334	0.320	1,500	4,000	0,750	006*0	1,800	1.600	0.125	2,000	0.800	0,665	4,000	0,250
PROJECT SECONDARY (CONT'D)	MARKHAM VILLAGE	MOORE TWP.	NEPEAN TWP.	NORTH BAY	ORANGEVILLE	PORT COLBORNE WS	PRESTON	RICHMOND HILL	SIDNEY TWP.	SIMCOE	STREETSVILLE	TILLSONBURG	WATERLO0	WESTM INSTER

NA - NOT AVAILABLE

DIGESTER OPERATION

As can be seen from the tables and graphs pertaining to digester operation, limited data is available. Much of the data provided is questionable with regard to its accuracy, partly due to the infrequent sampling and partly due to probable inaccuracies in meters.

Of the thirty plants utilizing digestion facilities only two provided all of the information required for a proper analysis of the performance. With regard to solids measurements, it was possible to obtain material balances (within 10 percent) on only six installations. This makes it difficult to place much confidence in the loading figures determined from the information supplied.

As indicated on Graph. 12 none of the digestion systems were designed for loadings in excess of those recommended in the WPCF Manual No. 8 although the actual loadings on the Owen Sound, Brampton and Brantford digesters were above this. In addition the design loadings on the primary digesters were in excess of the manuals recommendation at Brampton, Kitchener and Lakeview and the actual loadings were in excess of these recommendations at Owen Sound, Brampton, Brantford, Kitchener and Lakeview.

The effect of digester loading on digestion is shown on Graph. 13. This graph is not complete in that only seven plants are shown and this reflects the lack of information available. However, with the exception of the Point Edward unit it is indicated that the volatile content of the digested sludge increased with an increase in the load on the digester. It is noted in the WPCF Manual No. 9 that a well digested sludge should have a volatile content of approximately 50 percent or less. Based on this criteria and the loadings experienced at Kitchener, Lakeview and Brantford; a well digested sludge was not produced at these plants.

Although the loading at Point Edward was not high the volatile content of the raw sludge was above normal and this may in part account for the high volatile content of the digested sludge. Also, the temperature maintained at the digester and the amount of mixing employed should be reviewed.

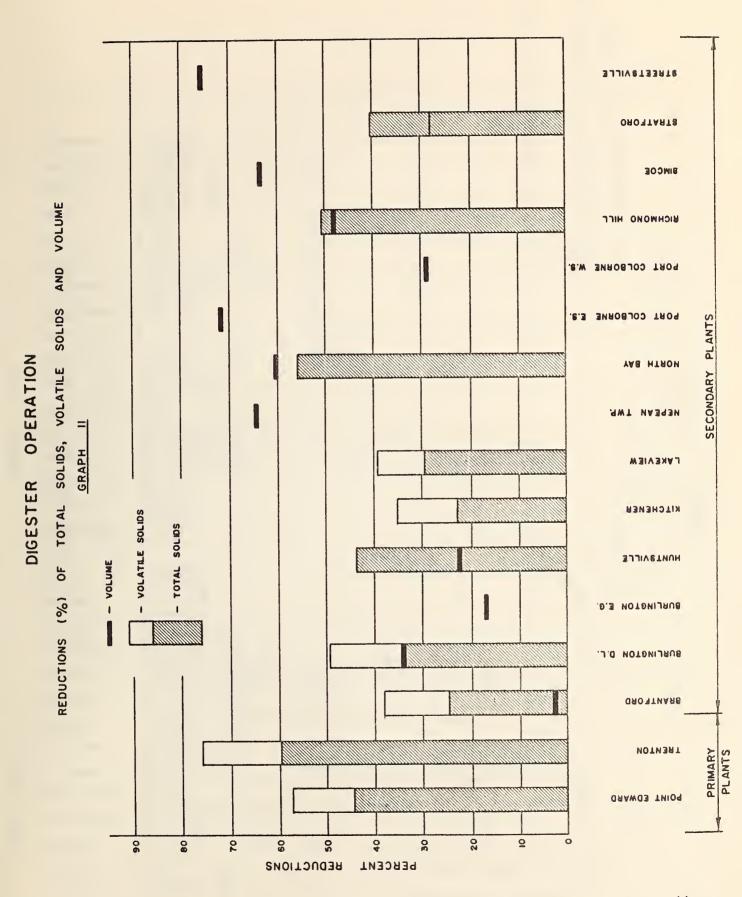
In general it is necessary to review the sampling program and the metering associated with the digestion process at the various plants if reliable information is to be obtained.

FRODUCTION LB FT ³ /LB EED VS RED		110		11 1118
GAS FRO FT ³ /LB VS FEED		1 1 1 1 1		6.4.0 0.4.0 0.4.0 0.4.0
U L T \$ VOLAT!LE CONTENT DIG_SLUDGE	2111101	4 - 38 - 1 -	1 1 1 1 1 2 4 1 1 1 1 1 1 1 1 1 1 1 1 1	11 11 10 11
R E S VOL.	111114	85 4.2 34 17	1 1811188 40	28 28 47.7 63.8 81.1 74
U C T I		38.8	1 11881 11	11 111411
R E D	11114	24.2	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11 01 17
0 T A L (LE/FT ³ /54Y)	0.035	0.019	0.053	0.00 0.00 1.00 0.00 0.00 0.00 0.00 0.00
1 N G T O T A (FT3/CAP) (L	2	, , , , , , , , , , , , , , , , , , ,	o word ii	0 0400 11 6 - 604
L 0 A D (LE/FT ³ /DAY)	0.069	0.038 0.30 0.287 0.074	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
АОТСА L РКІМАКУ (FT ³ /CAP)	1.25 1.75 1.12	11.001		1 1 0 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
		,		
ά L (LB/FT3 /DAY)	0.063 0.050 0.050 0.038 0.038	0.044 0.078 0.103 0.053 0.053	0.027 0.034 0.077 0.077 0.086 0.077 0.086 0.086	00000000000000000000000000000000000000
9 A D 1 N G	_	,	. ดูงบุบบุย ข.ง 4.0 . ดูงบุบบุย ข.ง 4.0 . ดูงบุบบุย ข.ง 9.0 . ดูงบุบบุย ข.ง 9.0 . ดูงบุบบุย ข.ง 9.0	· ·
S 1 G N L E A R Y (LE/FT ³ /DAY)			0.034 0.034 0.038 0.038 0.054 0.057 0.057	-
D E FT 3/CAP)				2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
DESIGN DE FLOM (MGD) (FT ³ /CAP)	6.00 6.00 6.00 6.00 6.00 6.00 7.00	2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	1.55 1.55 1.55 1.55 1.55 1.55 1.55 1.55 1.55 1.55 1.55	2000 2000
TYPE	222222	ASZD ASZD ASZD ASZD ASZD ASZD ASZD ASZD	ASID ASID ASID ASID ASID ASID ASID ASID	48.20 48.20
REMARKS	∢ ∪ ໝ ໝ ໝ <mark>ໝ</mark> ພ	n n n n n n n n n n n n n n n n n n n		4 mmm m 4
PROJECT	-46460000	o o o = o o 4 to d	18855B582522	**************************************
39				

29. PORT COLBOONE WS 30. PRESTON 21. RICHYOUS FILL 30. SIDNEY IMP.

36, TILLSOWEURG 37, MATERLOG 36, MESTMINISTER

33. SIMCOE 34. STRATECED 35. STREETSVILLE



DIGESTER LOADINGS

34

BRANTFORD 28 .26 .24 DIGESTED SLUDGE LAKEVIEW 22 KITCHENER PRIMARY DIGESTER LOADING €. GRAPH 13 VOLATILE CONTENT OF 4 DESIGN LOADINGS 77 STRATFORD 90 BURLINGTON D.L.X 9 TRENTON POINT EDWARD 40 02 0 69 64 62 00 56 48 46 44 58 54 52 တ္တ VOLATILE CONTENT OF DIGESTED SLUDGE (%)

PRIMARY DIGESTER LOADING - LBS. / ft./day

VACUUM FILTRATION

During 1964, the OWRC operated 8 filters at 6 of its plants. The types of sludge filtered at these installation was varied as shown in the table below:

Project	Design Flow MGD	No. of Filters	Type of Sludge	Filter Area Sq. Ft.	Filter Media
Brantford	12.5	2	P-A-D	700	Coil Springs
Galt	5.0	1	P-A-D	380	Plastic Cloth Media
Kitchener	13.5	2	P-A-D	500	Coil Springs
Preston	1.8	1	P-A-R	250	Coil Springs
S. S. Marie	8.0	2	P-R	400	Coil Springs
Waterloo	4.0	1	P-A-R	300	Coil Springs

P - Primary

A - Waste Activated sludge

D - Digested

R - Raw

All of the stainless steel coil spring filters were manufactured by Komline-Sanderson Limited. The filter at Galt is fitted with various plastic cloth media.

CHEMICAL DOSAGES

Graph No. 14 indicates the dosages of lime and ferric chloride as percent by weight of dry solids filtered.

PRESTON

The chemical dosages at Preston show a wider, but generally lower range than values given in the FSIWA Manual #8. The yearly average of both lime and ferric chloride are quite low and is indicative of the excellent filter results.

WATERLOO

The chemical dosages at Waterloo show a wider range than values given in the FSIWA Manual #8. The average annual dosage of ferric chloride is close to the range, but the lime dosage is well above normally accepted values.

BRANTFORD

The chemical dosages at Brantford vary over a very small range indicating that the quality of the sludge is quite consistent. The average lime dosage was slightly over the range of values according to the FSIWA Manual #8.

GALT

The chemical dosages at Galt show the widest range of all the plants and the average annual values were well above the normally accepted values. Operation of the Galt vacuum filter as indicated by the chemical dosages was very difficult. Many different types of filter cloths were tried in an attempt to normalize the filtering process.

KITCHENER

The chemical dosages at Kitchener varied over a wide range and the average annual chemical dosages were extremely high.

The operation of the vacuum filters became extremely difficult when the change from primary digested to secondary digested was made.

SAULT STE. MARIE

Chemical dosages improved during the year for the Sault Ste. Marie filters.

Although the dosages varied over a wider range than is normally expected the average annual dosages fell within acceptable values.

YIE LDS

The filter yields at each of the plants are shown on Graph No. 15. Each of the plants filtering undigested sludge obtained yields within the range given in the FSIWA Manual #8, with the exception of Preston which gave exceptionally good yields. The excellent yield from the Preston filter is undoubtably due to the heavy nature of the sewage solids which are quite high in starch.

The three plants filtering digested sludge all obtained yields much below the expected ranges in spite of having feed solids of normal consistency. An investigation into the reasons for these low filter yields will be initiated.

OPERATING COSTS

The total costs of the sludge filtering and disposal operations and the cost on a per ton basis are indicated in Table VIII .

The cost of filtering sludge varied from \$5.00 per ton at Sault Ste. Marie to \$20.54 per ton at Galt. Costs for labour, electricity and maintenance have been somewhat arbitrarily determined because of the difficulty of determining exact costs for all of the ancilliary equipment.

OWRC WATER POLLUTION CONTROL PLANTS

VACUUM FILTRATION

1964

F AR AV	3,04	2,60	2,44	7.0	9,43	4,50
YIELD ESF MONTHLY MAX MIN	3,55 2,31	3,86	3,21	0°0 2°0	12,60	5.80
S CAKE YEAR AV.	16.5	26.,7	17.8	27.1	25.2	
% SOL IDS MONTHLY MAX MIN	17.3	41.2	22.5	32. 2 22.0	27.2	
3 YEAR AV °	2,88	7.15	6.15	.0 .98	1.37	2,41
% FE CI MONTHLY MAX MIN	3,76	11,50 5,68	7,50 3,99	2,40	2,76	3,53
CL3 YEAR TOTAL	70.84	3,81 '4! , 54	2,06 108,58	5,20	25.60	16°99
OF FE AV.	5,90	3,8	12,06		2,13	4°.74
TONS OF MONTHLY MAX AV	7,52	7.42	18,32		3,79	3.16
IE VEAR AV•	13,7	24.4	23.1	2,4	7.1	10.7
% LIME MONTHLY MAX MAX	5 5 5 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	49.0 3.6	26.1	8 °C	12.0	17.1
IE YEAR TOTAL	28,01 335,10	13,65 150,15	44.80 403.24	12.68	132.10	21.01 252.12
OF LIN	28,0	13,65	44,80		Ç	21.01
TONS MONTH!	88 88 88 88	21,88	61,13		17,00	25.42
SOL IDS YEAR TOTAL	205,111 2461,35	626.97	32,67 1734,05	528.74	155,43 1865,16	96,63 2359,54
V AV	205,11	57,00		44°06		
TONS MONTHI MAX MIN	239,90	28.95	280.10	53,68 26,04	192,38	283,17
IN FEED YEAR AV	5,16	4,92	4.10	6,80	6.19	5.50
% SOL IDS MONTHLY MAX MIN	5,57	3,80	3,10	9.20	8,80 3,20	6,80
	2350	103,02 1133,25	2908,3	617,02	1077,5	3309.1
RING	195.8	103.02	323.1	51.4	89	275,8
HRS. FILTE MONTHLY MAX AV	N 90	30.00	417.0	38.0	154.0	330.5
PROJECT	*	\$ Z	× × ×	4	ر د	9

PROJECTS | BRANTFORD * 2 FILTERS IN USE

2 GALT * BASED ON 11 MONTHS ACTUAL

3 KITCHENER ** BASED ON 9 MONTHS ACTUAL

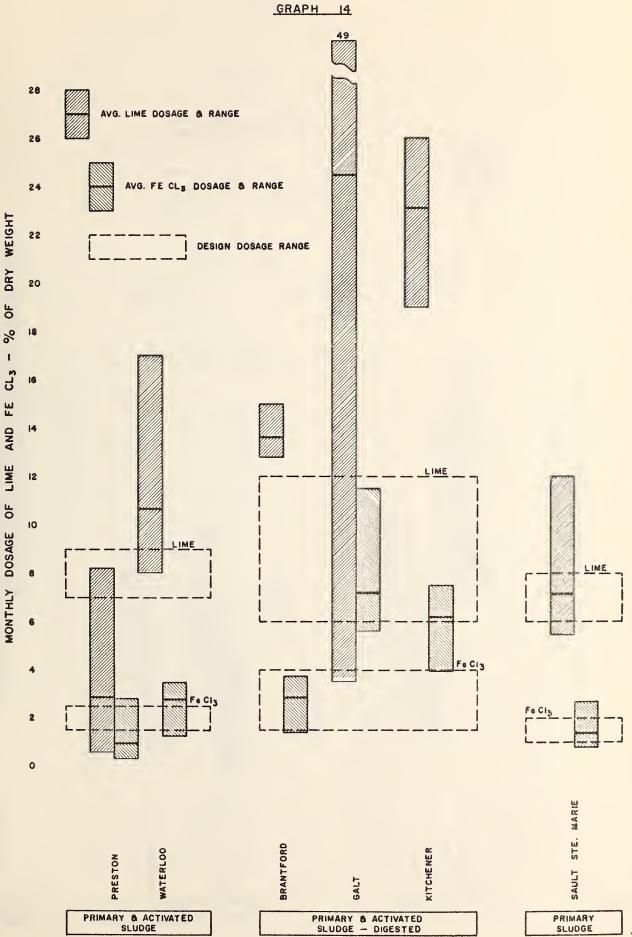
4 PRESTON B 6 MONTHS ACTUAL B 11 MONTHS ACTUAL

5 SALLT STE. MARIE

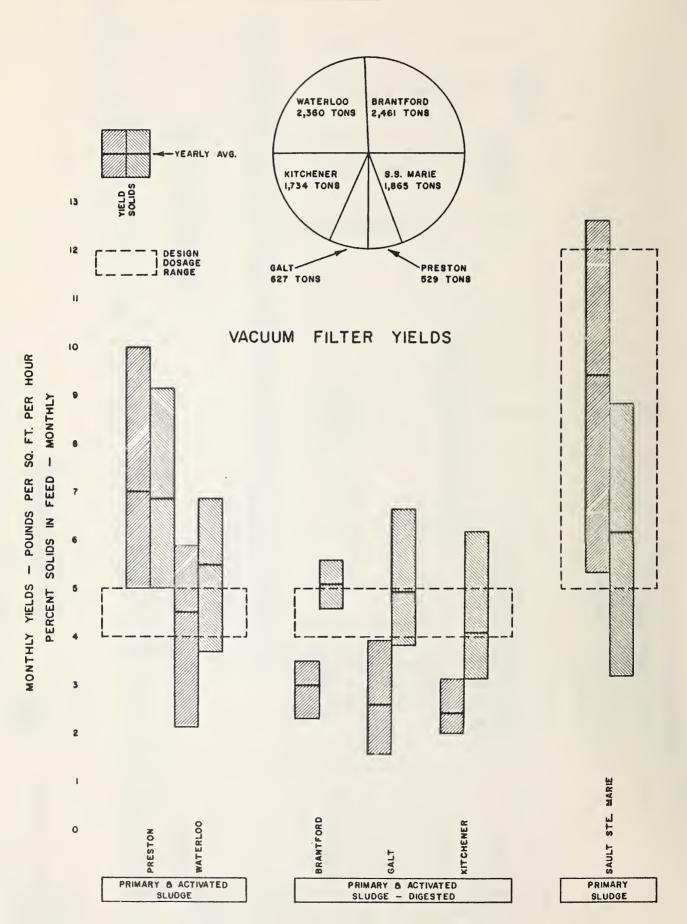
6 MATERLOO

TABLE VII

VACUUM FILTRATION CHEMICAL DOSAGES - % DRY WEIGHT



TONS OF DRY SOLIDS FILTERED 1964 GRAPH 15



O W R C WATER POLLUTION CONTROL PLANTS

TABLE VIII

VACUUM FILTRATION

1964

TOTAL FILTRATION COSTS

PROJECT	LABOR	ELECT	Fe Cl. 3	LIME	MAINT	TOTAL	TONS/YR	DISPOSAL
BRANTFORD	4599.96	3446.00	9136.90	5915.33	1232.00	24330,19	2461	6500.00
GALT	3150.00	626.97	5470.85	2627.60	1000.00	12875.42	627	3079.60
KITCHENER	5778.00	1733.00	14142.00	7054.00	747.00	29454.00	1734	12400.00
PRESTON	2000.00	528.72	676.05	221.03	500.00	3925.80	529	1638.00
S. S. MARIE	4905.00	1865.16	4274.77	2311.74	746.00	14102.67	1865	9570.00
WATERLOO	7350.00	2360.00	7407.00	4410.00	1500.00	23027,00	2360	13302.42
	THE REAL PROPERTY OF THE PERSON NAMED IN COLUMN TWO IS NOT THE PERSON NAMED IN			The same of the sa		The state of the s		

COST PER DRY TON FILTERED

PROJECT	LABOR	ELEC	Fe C1 3	LIME	MAINT	TOTAL	DISPOSAL	
BRANTFORD	1.89	1.37	3.75	2.40	0.50	9.94	2.64	
GALT	5.02	1.00	8.73	4.19	1.59	20.54	4.90	
KITCHENER	3.33	1.00	8.16	4.07	0.43	16.99	7.15	
PRESTON	3.78	1.00	1.28	0.42	0.95	7.42	3.10	
S. S. MARIE	2.73	1.00	1.22	0.64	0.40	5.99	5.13	
WATERLOO	3.12	1.00	3.14	1.87	0.64	9.76	5.85	



OPERATING COSTS

The total costs of operating sewage treatment plants as used in this report are those involving the payroll of staff employed at the plants, fuel, power, chemicals, general supplies, equipment, repair and maintenance, sundry and water. The cost of head office supervision, including travel, accounting, purchasing and inspection is not included in the operating costs shown for each project.

An explanation of items included in each of the categories of the operating costs is as follows:

- 1. Payroll Regular operators' salaries including pension and Workmen's Compensation payments.
 - Casual payroll Salaries of labour employed on a temporary or part-time basis in time of staff shortage or for part-time work.
 Workmen's Compensation payments are also included.
- 2. Fuel Includes fuel oil, natural gas, and/or propane used for heating.
- 3. <u>Power</u> Includes hydro electric power and natural gas, gasoline, diesel oil if used for power generator.
- 4. Chemicals Includes chlorine, ferric chloride, hydrated lime, pickle liquor, alum, sodium hypochloride, odour control chemicals, activated carbon, sodium chloride, pipe cleaning materials (where applicable).
- 5. <u>General Supplies</u> Includes laboratory reagents, laboratory equipment replacement, cleaning materials, lubricants, stationery, uniforms, light bulbs, instrument charts, books.
- 6. Equipment Includes equipment to be used in the treatment process, laboratory, building and grounds and small tools.

- 7. Maintenance Includes goods and services (with the exception of OWRC staff)
 used in repairing and maintaining process, electrical and
 building equipment, inspections, packing, paint, etc.
- 8. Sundry Includes express charges, telephone, telemetering, stamps, sludge haulage, etc.
- 9. Water Includes all charges for water.
- Includes operators' travel to local hardware stores, railroad station, conferences, conventions, etc. The cost of accommodation and meals associated with conferences and conventions is also included.

The major contributor to the cost of operation was payroll. On primary treatment plants the payroll costs averaged 42.1 percent of the total operating costs and ranged from a low of 32 percent at Trenton to a high of 57 percent at Fort William.

On secondary treatment plants the payroll costs averaged 45.2 percent of the total operating costs and ranged from a low of 25 percent at Lakeview to a high of 62 percent at Brantford.

POWER COSTS

The cost of power as a percent of total operating costs and on a per million gallon basis is shown on Tables XI and XII.

Power costs for primary treatment plants varied from 11 to 20 percent and averaged 15.4 percent. Power costs for secondary plants varied from 6 to 40 percent and averaged 17.2 percent.

Power costs per million gallons treated are shown on Graph No. 19 . The graph shows a very wide range due to differences in pumping, vacuum filtration and flows in the smaller plants, but stabilizes somewhat in the larger adequately loaded plants.

The Burlington Skyway plant shows an extremely high power cost because it is underloaded, has an inplant pumping station and is designed to operate now as a total oxidation plant, but eventually to change to a large conventional plant.

The Waterloo plant shows a high power consumption because of the extremely high BOD and SS loads and the continual operation of the vacuum filter.

MAINTENANCE COSTS

The cost of maintenance as a percent of total operating costs and on a per million gallon basis is shown on Tables XI and XII.

Maintenance costs for primary treatment plants varied from 4 to 23 percent and averaged 9.6 percent. Maintenance costs for secondary treatment plants varied from 6 to 22 percent and averaged 11.6 percent.

Maintenance costs per million gallons treated are shown on Graph 20.

The graph shows a very wide range due to differences in flows, amount of equipment and age of the plant, but stabilizes somewhat in the larger adequately loaded plants.

The Burlington Skyway plant shows an extremely high maintenance costs because of the large amount of equipment and the low flows.

SLUDGE DISPOSAL

The cost of disposal as a percent of total operating costs and on a per million gallon basis is shown on Tables XI and XII. .

Sludge disposal costs for primary treatment varied from 1 to 13 percent and averaged 5.2 percent of total operating costs. Sludge disposal costs for secondary treatment varied from 3 to 39 percent and average 12.8 percent.

Some plants showed nil sludge disposal costs for the following reasons:

- 1. Initial year of operation and no sludge to be disposed of.
- 2. Sludge drying beds or lagoons and removal by plant staff or public.
- 3. Removal at no cost by municipality.

The highest sludge hauling costs occurred at the Lakeview plant where the large volumes of sludge and the necessity to haul it longdistances made the hauling costs extremely high. All plants with vacuum filters will show an artificially low disposal cost because sludge is thickened prior to disposal.

OPERATING COSTS

SECONDARY TREATMENT	L											
PROJECT	TOTAL	PAYROLL	CASUAL PAYROLL	<u> </u>	POWER	CHEMICAL	SUPPLIES SUPPLIES	E SOLE	REPAIRS & MAINT.	SUNDRY	WATER	TRAVEL
NOTOWAR	41, 489,00	11.564.01	4701.95	122,32	5718 DB	3310.16	928-06	5022 5022	1479. EE	6050 58	1141.79	341,00
COCALMAN	171,859,76	104, 430, 57	2715.03	95.4 VR	23489 09	8533,45	2893, 22	2000	(540, 79	00 000	2380 84	202 20
RIGHT BUCKON D. L.	45,025,90	03.011.79		90.61	7469.04	4314.06	876.35	1000	1382, 35	6,60 82	280 66	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	21,957,56	10,355,83		982.74	3774.38	272.23	200	420 42	1385 14	3353 07	200 200 200 200 200 200 200 200 200 200	000
	43, 402, 99	14,318,02			17391,76	1340,20	1589, 70	2070.47	851.43	400000	361 74	14.00 17.00
	11,738,97	4,733,05	1071.50	729.31	1114.89	324.24	369,55	1868, 968	1200	201.00	1	717.30
FERGUS	19,881,89	8,623,87		371.96	1184,72	135,41	747,23		287,780	4:96.49	552, 96	168.76
GALT	77,875,88	32,720,37	1718.22	2550,84	7689,72	18911010	1792,47		3433.00	6707.82	1263,00	200
GEORGETOWN	29,738,15	13, 133, 49	515,51	121.51	3484,72	923,02	1484,43	493,43	2077/337	4998,55		490,55
HUNTSVILLE	10,121,07	4,016,47	312,14	411,53	1263,54	240.02	485,51	88,62,8	546,84	2165.00	387,61	C.C. 7
KINGSTON TWP.	23,296,77	9,086,55	300,43	1452,22	6460,77	09,109	1004,24	1145,83	40C.63	2195,10		649,40
KITCHENER	217,424,52	81,465,05	6798,20		34042,25	31838,33	3950,06	3803, 72	\$6594,97	38611.10	352,35	558,49
LAKEVIEW	159,677,53	32,457,67	8755,48	516.40	19312,41	9340,36	3372,61	3286.84	3443.4)	78368,06	703,65	120,65
MARKHAM VILL.	15, 120,53	8,984,45		779,91	1946.07	63,06	617,99	687, 49	536,46	793,61	582,59	128,90
MOORE TWP.	10,546,67	4,569,61	232,20		3581,00	311,79	507,06	550,41	444,70	187.43	142.47	20.00
NEPEAN TWP.	31,159,12	11,648,16	1209,96	332.07	8027.4	889, 15	909,21	501.50	4951.17	1470.39		220.10
NORTH BAY	72,953,91	30,506,95	1719,78	76,77	10024,18	1564,32	2815,02	673,97	5031.25	16869,55	3199,99	472
ORANGEV ILLE	13,000,89	4,532,77		195,61	1441.08	1705,38	216,60	45.44	456.81	4307,20		
PORT COLBORNE E.S.	57,818,45	38,627,06	207,24	1502,35	3916,57	67,017	2810,00	180,35	1021-11	3420.76	373,38	*692.45
PORT COLBORNE W.S.	+											
PRESTON	30,646,67	13,617,59	474,34	533,71	4917,83	1620,07	1109,62	842,73	1261,44	3420,63	2667,07	184,64
RICHMOND HILL	51,048.81	16,518,15	3994,37	1142.04	6569,64	5463,97	1011,62	185,95	2066,21	13697,06		399,80
SIDNEY TWP.	6,024,26	2,007,24	746,28	598,09	1098,31	317,55	273,15	141,93	22,48	287,22		532,00
SIMCOE	33,517,36	15,213,49	2742,56	1190.77	7731.81	814,98	1459,19	2214,44	1228,04	361,32	385.46	174,90
STRATFORD	53,649,88	26,699,97	2580,35	69,35	5901.60	95,38	2465,36	595,36	4197,95	10173.17	625,74	245,65
STREETSVILLE	14,024,94	4,110,24	2825,73	787,83	1475.77	441.01	487,36	80,63	937,01	2651.75	227,61	
TILLSONBURG	21,844,08	8,614,38		134,13	5157,89	158,04	880.04	505,95	1481,69	4547,06	229,90	125,00
WESTM!NSTER	10,784,36	4,480,26	633,83	1/30,033	2602,78	20.012	316,42	49,99	981,14	19479,15		561.15 243,90
		,						Description of the second seco			*	
PK MAK TEALMEN				The state of the s							COMBINED COST	:0 cos
BELLEVILLE	41,246,10	13,690,11	0	1100,59	7,9422,65	730.54	1351,51	120.01	1217,71	13859,63	1162,75	590,60
ESPANOLA	7, 109.88	2,556,22	44, 10	838, 18	1,418,03	(23°87)	244,59	/8° 30	7007	1393,40	0	270
FORT ERIE	23,886,73	9,822,35	223,28	1566,94	4,650,16	1616,84	1198,55	65 1 286	158, 10	3678,76	8	289,83
FORT WILLIAM	30,424,60	16,321,27	768,40	1952,50	5,344,30	3329,92	1384,55	665,50	108,80	391.04	81,00	47.32
DWEN SOUND	27,331,80	11,177,95	1721,61	1339,63	4,905,91	119,81	772.47	755,88	1028°28	3725,93	1492.07	292,25
POINT EDWARD	12,451,09	5, 103,63	0 -	1404.51	885,66		296.53	550,05	419,10	1917,86	1543,67	176.65
PORT ARTHUR	45,374,87	15,560,48	5023,02	1216,94	5,289,56	4.5	6220°20	369°36	2526.80	8205,96	2281,88	360,72
S.S. MARIE	112,623,50	49,515,17	984,40	25.45.20	16,555 ,5 3	C 33	2472,50	1251.40	5046,98	19907, 11	2249,42	264,60
TRENTON	18,422,16	5,083,11	650,88	464,34	2,413,87		705,45	105,00	3761,86	1476,36	1139,29	269,80
Con. or. oraclemental and an article of the control												

OPERATING COSTS

1964

SECONDARY PLANTS

PROJECT	TYPE	DESIGN	OPERATING CGSTS	COST / M.G.	COST / LB. B.O.D.	COST / LB S.S.
BRAMPTON BRANTFORD EURLINGTON D. L. BURLINGTON E. G. BURLINGTON SKY. CONISTON FERSUS GALT GEORGETOWN HUNTSVILLE KINGSTON TWP KITCHENER LAKEVIEW MARKHAM VILLAGE MOORE TWP. NORTH BAY DRANGEVILLE PORT COLBORNE W.S. PRESTON RICHMOND HILL SIDNEY TWP. SIMCOE STRAFFORD STRAFFORD STREETSVILLE TILLSONBURG WATERLOO WESTMINSTER	\$ 3 5 5 5 0 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2,000 12,500 2,500 0,750 3,125 0,260 0,600 1,500 0,250 0,33 13,500 5,000 0,334 0,320 1,500 4,000 0,750 0,850 0,900 1,800 1,600 0,125 2,000 4,000 0,800 0,800 0,250	41,489.00 171,859.76 45,025.90 21,957.56 43,402.99 11,738.97 19,881.89 77,875.88 29,738.15 10,121.07 23,296.77 217,424.52 159,677.53 15,120.53 10,546.67 31,159.12 72,953.91 13,000.89 (57,818.45) 30,646.67 51,048.81 6,024.26 33,517.36 53,649.88 14,024.94 21,844.08	51.10 77.39 54.65 93.24 160.15 178.28 110.37 41.09 96.82 159.75 214.34 71.84 67.69 179.62 329.38 42.89 59.10 69.38 (135.88) 107.80 108.10 63.02 69.06 53.95 81.39 116.50 131.74 205.54	0.01 0.06 0.02 0.08 0.09 0.04 0.03 0.10 0.12 0.43 0.02 0.03 0.07 0.17 0.07 0.17 0.07 0.017 0.08 (0.17) 0.02 0.08 0.10 0.02 0.03 0.06 0.10 0.02 0.03 0.03 0.06 0.16	0.06 0.05 0.02 0.05 0.07 0.10 0.04 0.03 0.06 0.09 0.21 0.02 0.03 0.05 0.18 0.08 0.02 0.08 0.02 0.06 (0.13) 0.02 0.04 0.05 0.03 0.05 0.03 0.02 0.04 0.05 0.03 0.09
VERAGE				1:1.79	0.08	0.06

PRIMARY PLANTS

PROJECT	DESIGN CAPACITY MG	OPERATING COSTS	COST/ M.G.	COST/ LB. B.O.D. REM'D \$	COST / LB S.S. REM'D \$
BELLEVILLE ESPANOLA FORT ER!E FORT WILLIAM OWEN SOUND POINT EDWARD PORT ARTHUR SAULT STE. MARIE TRENTON	3.0 0.665 1.8 6.0 3.0 0.57 4.0 8.0	41,246.10 7,109.88 23,886.73 30,424.60 27,331.80 12,451.09 45,374.87 112,623.50 18,422.16	22,00 129,51 46,57 37,11 23,82 186,88 27,52 46,29 99,980	0.025 0.235 0.180 0.030 0.230 0.040 0.120 0.125	0.010 0.059 0.111 0.020 0.082 0.025 0.046 0.800
everage			68,85	0,123	0.144

O W R C WATER POLLUTION CONTROL PLANTS

PRIMARY TREATMENT OPERATING COSTS

1964

PROJECT COSTS SELLEVILLE Al, 246, 10 ESPANOLA 7, 109,88 FORT FRIF 23,886,73		B - 2										2000
		20 8			20 %			800			S OF	
×	TOTAL	TOTAL	DER M.G.	TOTAL	TOTAL	S DER M.S.	TOTAL	TOTAL	C W	TOTAL	TOTAL	A DEG
*	13,690,11	33,2	7,28	7422,65		3,95	2689,23	6.5	1,43	520,38	0-1	0.28
_	2,600,32	ું	15,79	1418,09	20.02	8,61	325,49	্প	80	592,80	8	3,60
_	10,075,63	42.0	19,64	4650.16	0.61	9,07	2008,51	0	3,92	314,08	0	900
¥.	17,089,67	57.0	20,85	5344,30	17.0	6.52	2538,85	350	2,63	Z		
	12,889,57	47,2	11.24	4905,91	17.9	4,28	2556,53	(a)	2,23	731.11	2.7	0.64
POINT EDWARD 12,451,09	5,103,63	_	09°92	885,66	7.	3,29	1255,58	0.00	00.01	280,80	. 0	4 20
PORT ARTHUR 45,374,87	20,583,50	-	8	5289,56		65	4116	C	000	58.56.60	, v	. S. S.
S.S. MARIE 112, 523,50	50,499,57	_	20,76	16555,53	S. S.	200	8770.88	C 00		2750 00	ູ່ ຕິ	t c
	5,733,99		31.12	2413,87	000	13,10	4572,31	200	000) o	200
								no-ma		9		
		-,-							A COLUMN TO SECURE OF SECU	The second secon		The state of the s
AVERAGE		42.1			15.4			9.6			5,2	

* BASED ON ESTIMATED FLOW

LABOUR INCLUDES: PERMANENT & CASUAL

MAINTENANCE INCLUDES: GENERAL SUPPLIES , MINOR EQUIPMENT, REPAIRS & MAINTENANCE

1964

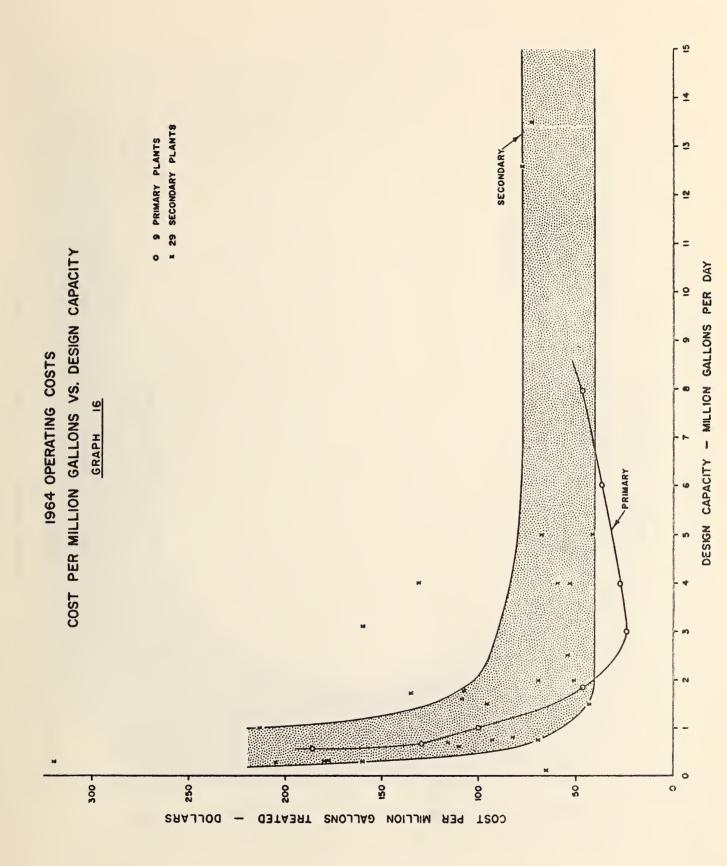
S E C O N D A R Y P L A N T S

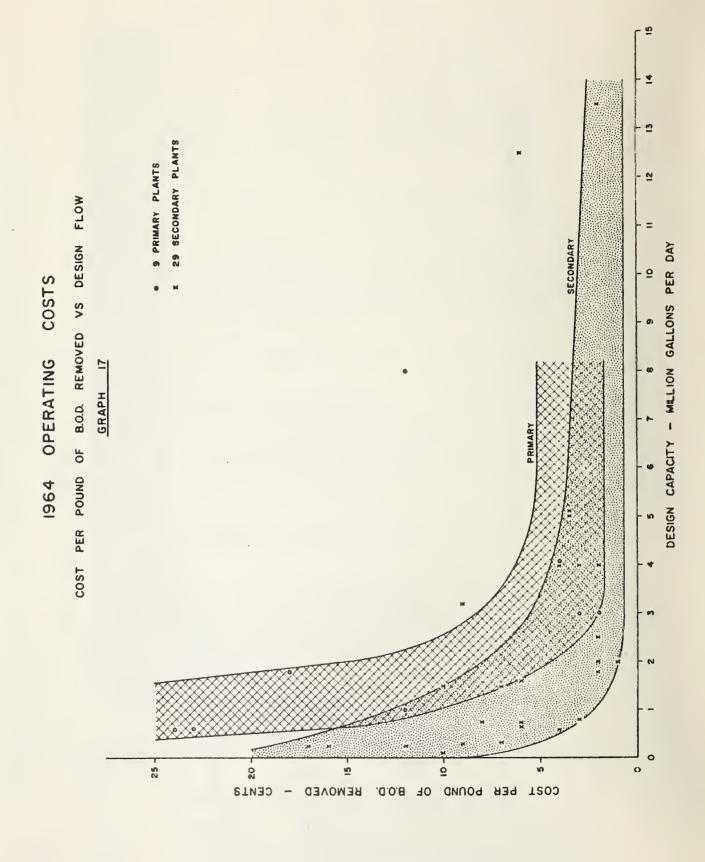
		A I	ABOR COSTS	U	MOd	POWER COSTS		MA	MAINTENANCE	21.	Stunge	GF DASPOSA	SA	
AO. EC.	OPERATING		% OF			30 %			40 %	li .		% OF		
	COSTS	TOTAL	TOTAL	₩ PER M°G	TOTAL	TOTAL	ಈ PER M ಿಂ	TOTAL		S PER M.G.	TOTAL	TOTAL	PER M.G.	
			Contract and					The state of the s			The second secon			
BRAMPTON	41,489,00	16,256,95		20,06	5718,08	14.0	7,006	7639,12	0.81	9,43	2545,20	6,1	3,5	
BRANTFORD		107, 145,50		48,24	23489,09	1307	85.01	9087,86	5,3	600	4980,32	0,0	2,24	
BURL METON D.L.		23,211,79	51,4	28, 18	7469,04	17.0	9.07	3320°37	0,0	4.03	3419,20	7.6	4.13	
		10,355,83		43,98	3724,38	17.0	15,82	2522,14	0.11	10.78	2069,94	0 0	8,80	
		14,318,02		52,83	17391976	40°0	64.17	5521,60	13,0	20,37				×
	11,738,97	5,844,55	50,0	88°76	1114,89	10.01	16,93	2687,68	22,0	40°82	Į. Z			4
FERGUS	19,381,89	8,623,87	43°0	47,88	1184.72	6.0	6,53	3547.78	18,5	80,82	12			
GALT	77.875.88	34,438,59	44.0	18,17	7689,72	0.01	4,06	6186,51	್ಯಿ	3,26	2693,40	605 803	3,5	
GEORGETOWN	29,738,15	13,649,00	ಿ.0	43,86	3434,72	<u>လီ</u>	11,35	5051,18	13,0	16,43	3675.60	12°5	11.97	
HUNTSVILLE	10,121,07	4,328,61	43.0	68,44	1263,54	0°2	19°93	1212,23	0.5	19,17	1308,66	ಬ್ಬ	50°69	
KINGSTON TWP.	23,2%,77	9,386,98	40.0	84.09	6455,77	28°	57,88	2550, 70	್ಟಿ		Z			
KITCHENER	217, 424,52	88,263,25	39°0	29,16	34042,25	0.91	11.25	24358, 75	್ಟಿ		12400,00	5.7	4,10	
LAKEVIEW	159,677,53	41,213,15	25,55	17.47	19312,41	12°0	යි වැ. ඉ	10:02,85	0,0		62,461.68	39, 1	26,48	
MARKHAW VILL.	15,120,53	8,984,45	59,5	166,73	1946,07	ري. د.	23, 12	1849,94	် (၂		2		- Carrier	
MOORE TWP.	10,546,67	4,801,81	45°3	96°571	3581,00	34.0	11300	1205	14°0	50° SF	್ಟ 2			4
NEGEAN TWP.	31,159,12	12,858,12		17,70	8027,41	19 19	11,003	6361.88	20°4	8,76				
NORTH BAY	72,953,91	32,226,73		26.11	10024, 18	3,5	8, 17	8520,24	12,0	06°9	13435,66	9,0	10.88	
CRANGEVILLE	13,000,89	4,532,77		24,19	1441.03	0	2,69	818,85	6,3	4.37	3277,06	25,5	17,49	
FORT COLBORNE E.S.	57,818,45	38,834,30	57.5	92.16	8916,57	15,0	20,05	4011,47	7°	9,43	1863,50	ഡ ന്	4,38	,
PORT COLBORNE W.S.	×													€-
PRESTON	30,646,67	14,091,93	45,5	49,56	4917,83	್ಯಿಂತಿ	8.7	3212,79	0,0	11,30	1638,00	ເລິ່	5,75	
RICHMOND HILL	51,048,81	20,512,52	40,2		6569,64	ر د د د د	3°0	3263,78	0,4	500	13467,000	4°07	28.52	
SIDNEY TWP.	6,024,26	2,753,52	45,0		1098,31	0,6	11.49	437,56	7.0	4.53	2		Bern Charle	*
SIMCOE	33,517,36	17,956,05	53,0		7731,81	23,0	5,63	4901.57	5.0	0,00	7 2			
STRATFORD	53,649,88	28,280,32	54,6		5901.60	Ç.	5.94	7258,67	3,5	7,30	7539,00	2	7,58	
STREETSVILLE	14,024,94	6,935,97	49.0		1475.77	0.1	8,57	1505,00	0°5	8,73	2331.25	9,9	က္က	
TILLSONBURG	21,844,08	8,614,38	39,4		5457,89	23,6	27.51	2867.68	3,8	5. 33 3. 33	4341.82	ත <u>ු</u>	23, 15	
WATERLOO	112,363,46	38,004,12	34,0		22579,02	20°0	26.47	8952,38	್ಯಿ	10,50	13715,66	12,2	16,08	
WESTMINSTER	10,784,36	5,113,50	45.5	97.46	2602,78	24.0	49,61	1348, 15	12,5	25,69	471.75	4.4	66,8	
AVERAGE			45.16	Section of the sectio	Active Specific Speci	17.2			11.6	Application of the second district of the second se	and the first many to the plant of the comments of the comment	12,8	A skriutele Kingelie in Application, skriutele für negelege spesieren.	
	THE REAL PROPERTY AND ADDRESS OF THE PERSON ADDRESS OF THE PERSON AND ADDRESS OF THE PERSON AND ADDRESS OF THE PERSON ADDRESS OF THE PERSON ADDRESS OF THE PERSON AND ADDRESS OF THE PERSON ADDRESS OF THE	A STATE OF THE PARTY OF THE PAR	76. LETNEL MEDICAL	- The manufacture of the same	TO THE RESIDENCE OF THE PARTY O		The second secon	THE RESERVE OF THE PARTY OF THE	-	THE CHANGE THE PARTY OF THE PAR	The second second second second	TOTAL SERVICE STATE OF THE SER	A Charles and a second parameters of the contract of the contr	ALCOHOLD SERVICE CO.

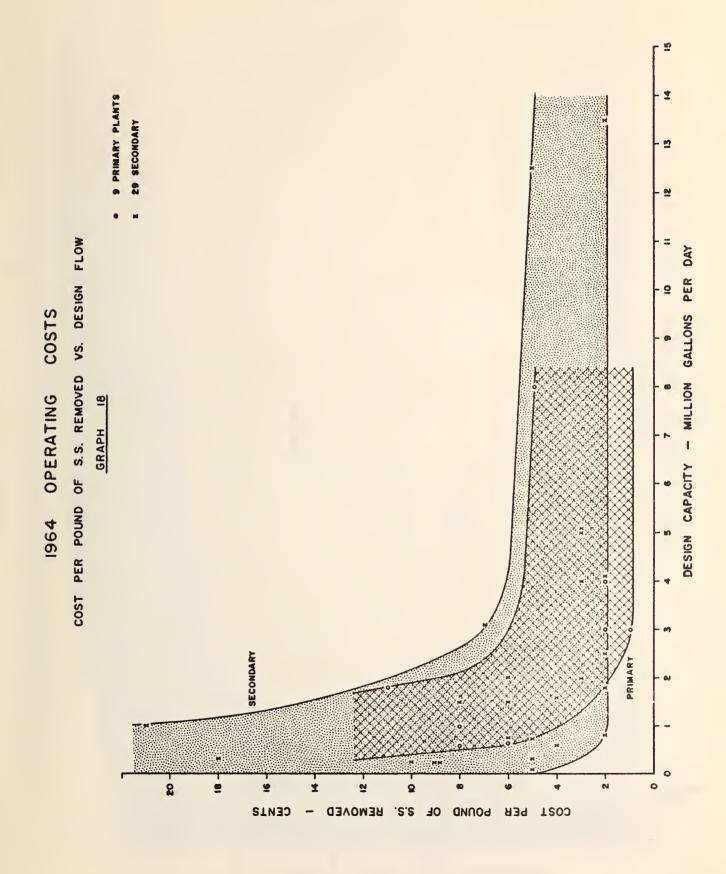
X COSTS BASED ON 4 MONTH'S FLOW

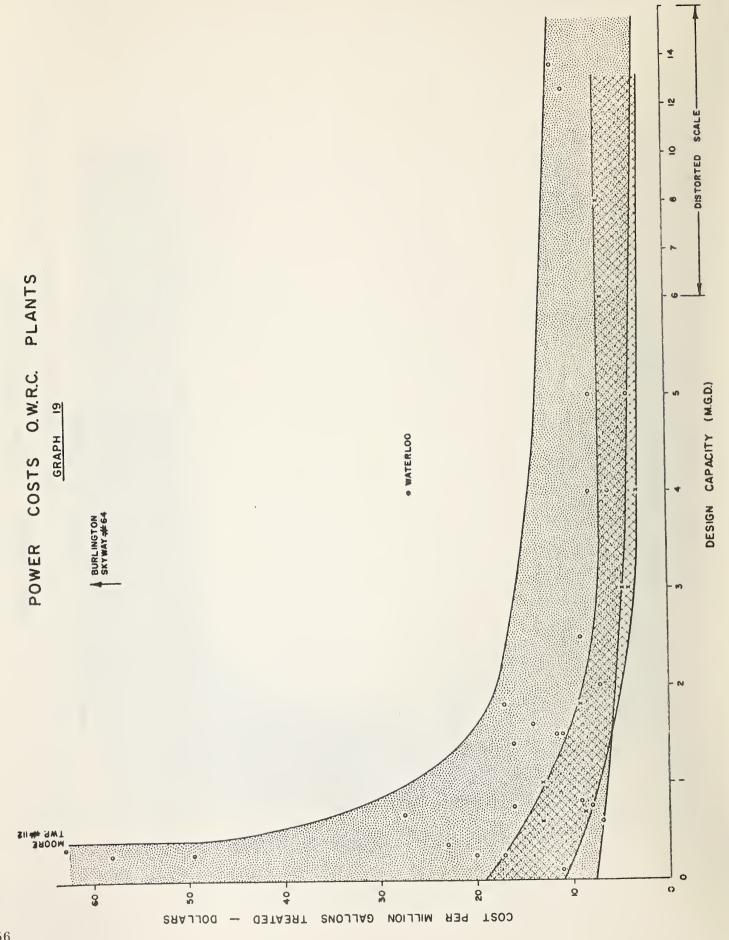
[♦] COSTS BASED ON PRO⊷RATED FLOWS

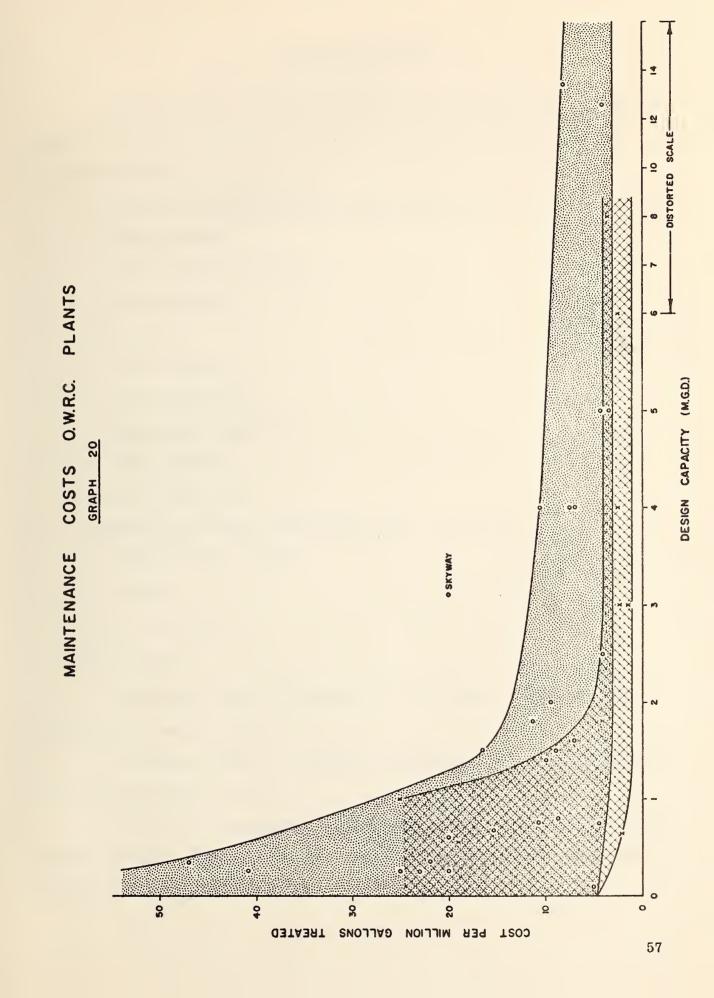
^{*} COMBINED COSTS.













OPERATING STAFF

During 1964, the Commission's 9 primary plants and 29 secondary treatment plants were operated by a total of 165.5 permanent employees and the equivalent of 7.5 casual employees.

There were 13 different classifications in effect as follows:

- 8 Superintendents
- 1 Assistant Superintendents
- 18 Chief Operators
- 6 Foreman
- 9 Plant Mechanics
- 3 Plant Electricians
- 2 Laboratory Technicians
- 2 Filter Operator
- 7 Senior Operators
- 94 Operators (Trenton & Sidney Twp. share 1 operator)
 - 7 Groundskeeper Janitors
 - 1 Clerk
- 7.5 Casual laborers

165, 5 TOTAL

Seven of the 38 plants were staffed with only one man. The largest staff was 22.5 men at the Brantford plant.

As indicated in Graph 21 most of the primary plants were staffed by about 1 man per million gallons of capacity.

The very small secondary plants, generally about a third of a million capacity, have one operator. Depending on local circumstances plants in the size range from 0.3 to 1 mgd are staffed with 2 operators.

The larger plants above a capacity of 1 mgd are staffed with between 2.5 and 1.5 men per MGD treatment capacity.

The Markham Village plant shows the highest staff complement on a men per mgd basis, because there are two operators and the plant only has a capacity of 0.334 mgd. There are 2 pumping manholes and 1 large on site pumping station associated with this project.

The Richmond Hill and Simcoe projects show a generally higher staff complement because the Richmond Hill project consists of 3 plants side by side and the Simcoe project 2 plants side by side.

PRIMARY TREATMENT PLANTS

1 9 614

PROJECT	TYPE	SUPER INTENDENT		⋖	PLANT MECHANIC		LAB. TECH.		OPERATOR	GROUNDS-JANIT.	CLERK	TOTAL	DESIGN CAPACITY M.G.D.	AVG. DAILY FLOW M.G.D.	MEN PER M.G.D. DESIGN	HOURS PER WEEK COVERAGE
			_													
BELLEVILLE	PP,DT			1					2			3	3,00	5.14	1. ₀ 0	48
ESPANOLA	DT								1			1				
FORT ERIE	PP		1	1					.1			2	1.80	1.05	09	44
FORT WILLIAM	PP, DT			ì	iŧ				.3	1		6	6,00	2.24	1.0	112
OWEN SOUND	PP		1	ı					2			3	3.00	3.13	10	48
POINT EDWARD	PP, DT								4			1	0.57	0.18	17	40
PORT ARTHUR	PP, DT		,	ı					2			4	4,00	4.51	1O	41/2
S. S. MARIE	VT	8			1		1		6	1		10	8.00	6,65	1.2	112
TRENTON	DT			ł					5,			1,5	1.00	0.50	1.5	44
TOTAL		1 () (5 C	2	:0 () 1	0	18.5	5 2	0 1	31.5				

CLASSIFICATION

P - PUMPING AT PLANT

PP - PUMPING IN SYSTEM & PLANT

D - DIGESTION

DB - DIGESTION & SAND DRYING BEDS

DT - DIGESTION & LIQUID TRUCKING

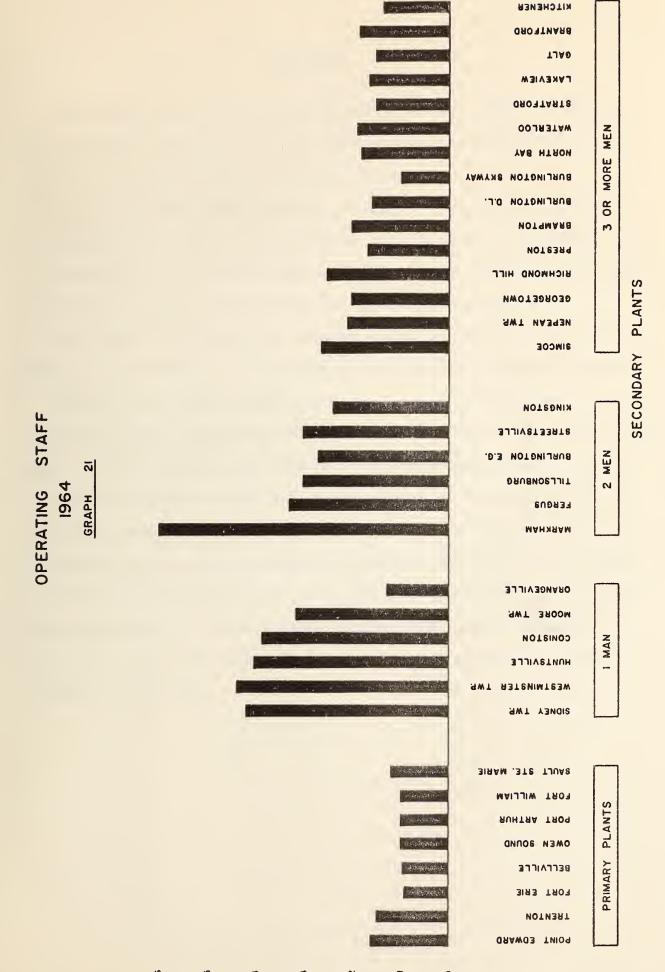
VT - VACUUM FILTRATION & TRUCKING

OPERATING STAFF

SECONDARY TREATMENT PLANTS

1964

	CLASSIFICATION											1			
PROJECT	SUPERINTENDENT	ASST. SUPER	CHIEF OPERATOR	FOREMAN D. AST. M.C. 18810	PLANT ELECT.	LAB. TECH.	FILTER OP.	SENIOR OP. OPERATOR	GROUNDS-JAMIT.	CLERK	TOTAL	DESIGN CAPACITY	AVG. DAILY FLOW	MEN PER M.G.D. DESIGN	Hours Per week Coverage
BRAMPTON BRANTFORD BURLINGTON D.L. BURLINGTON E.G. BURLINGTON SXY. CONISTON FERGUS GALT GEORGETOWN HUNTSVILLE KINGSTON TWP. KITCHENER LAKEVIEW MARKWAM VILLAGE MOORE TWP. NCRTH BAY ORANGEVILLE PORT COLBORNE E.S. PRESTON RICHMOND HILL SIMCGE SIDNEY TWP. STRATFORD STREETSVILLE TILLSONBURG WATERLOO WESTMINSTER		:		5	1 1	1	1	202-3525424-6 322566-	2	1.55 0.22 0.23 0.55	3 2 5 1 2 7 3 1 2 18 7 2 1 3 2 7 2 1 8 4 4 4 3 0 5 5	2.0 12.5 2.5 0.75 3.125 0.260 0.6 5.0 1.5 0.25 0.83 13.5 5.0 0.320 1.5 0.320 1.5 0.85 0.9 1.8 1.6 1.4 0.12 4.0 0.8 0.67 4.0 0.8 0.67 4.0 0.25	2.21 6.07 2.26 0.64 2.24 0.18 0.49 5.18 0.84 0.17 0.31 8.30 6.44 0.09 1.99 3.39 0.51 0.36 0.80 0.78 1.29 1.33 0.26 2.72 0.47 0.51 2.34 0.14	2.0 1.8 1.2 2.7 1.6 3.8 3.3 1.4 2.0 4.0 2.4 1.3 1.4 6.0 3.1 2.5 2.5 2.5 2.5 2.0 2.0 2.0 2.0 2.0 2.0 2.0 2.0 2.0 2.0	56 168 88 48 40 54 112 40 56 168 17 56 40 56 168 17 56 40 56 56 56 56 56 56 56 56 56 56 56 56 56
TOTAL	7	1	12	6 7	3	2	1	75.5	5 1	6.5	134				





SUMMARY

The purpose of this summary report is to compare a large number of individual plants operated by the Ontario Water Resources Commission and to reach some conclusions by comparing the plants under different categories.

It is most difficult to make a summary of a summary and arrive at many meaningful conclusions. The widely different designs of the many plants provided the opportunity of encompassing the whole sewage treatment field but there is the distinct disadvantage in not being able to compare plants under similar operating conditions.

Some of the categories studied revealed meaningful results because of the relative accuracy of the available data. Information on flows and operating costs are examples.

Generally most of the comparisons indicate wide ranges of values which can only suggest further study on those plants which are greatly different from the average. The lack of accurate information on digestion makes any conclusions impossible.

In spite of the many faults and ommissions revealed, a summary such as this is invaluable in assessing the actual operation of a large number of different plants. The fact that inaccuracies and ommissions can be revealed in this report is a justification in itself for producing such a report. It is only in this way that efforts can be directed toward improving the information available from individual plants so that efficient operation of the plants can be maximized and future summary reports can be made more meaningful and informative.

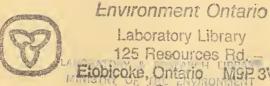


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ONTARIO WATER

TD 1964 operating summary: water pollution control plants. 367 .A56 81562 097 1964



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